

Worldwide Pollution Control Association

WPCA-Entergy
“Increasing Energy Efficiency of Existing Units” Seminar
January 22, 2014

All presentations posted on this website are copyrighted by the Worldwide Pollution Control Association (WPCA). Any unauthorized downloading, attempts to modify or to incorporate into other presentations, link to other websites, or to obtain copies for any other purposes than the training of attendees to WPCA Conferences is expressly prohibited, unless approved in writing by the WPCA or the original presenter. The WPCA does not assume any liability for the accuracy or contents of any materials contained in this library which were presented and/or created by persons who were not employees of the WPCA.



Visit our website at www.wpca.info



Efficiency by DryFining

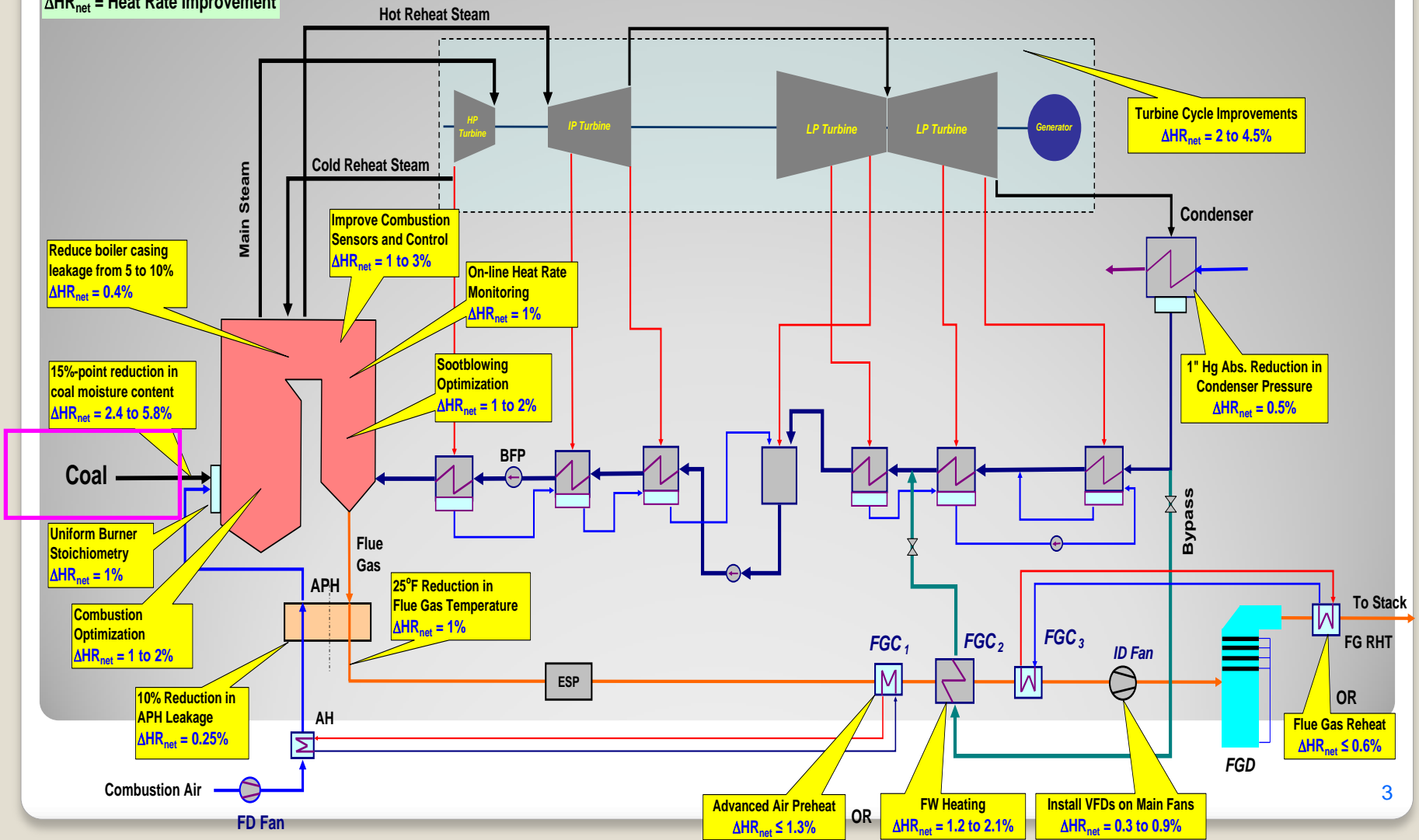
WPCA/Entergy Seminar
The Woodlands, TX
Charlie Bullinger, PE
Great River Energy

- Efficiency at Great River Energy
- Drying effects
- DryFinishing background: why and how
- Commercial installation
- Performance and benefits '09 thru '13
- Summary

Presentation Outline

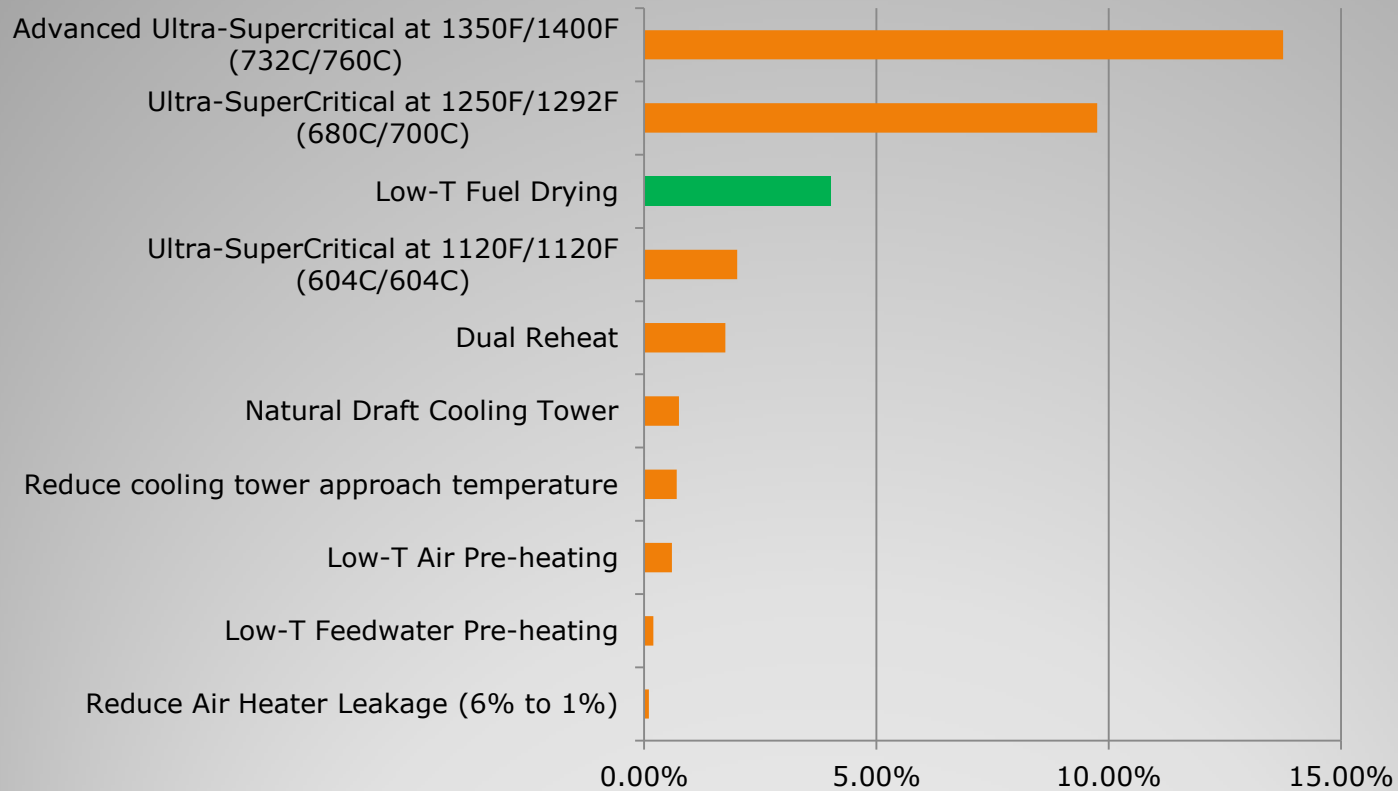
Heat Rate Improvement Opportunities

ΔHR_{net} = Heat Rate Improvement



- Turbine blades
- Cooling Towers
- Simulator
- Ventilation
- Variable packing
- Fans
- Controls
- Leak detection
- Compressed air
- 605,771 tons CO2
- Coal
Drying/beneficiation
- 4%, 400,000 tons

Efficiency Improvements: GRE



Heat Rate Improvement Technology Comparison

EPRI Report: 1015698,
CoalFleet Guideline for
Advanced PC Power Plants

Heat Rate improvement calculation

$$HR_{net} = \frac{HR_{cycle}}{\eta_B \left(1 - \frac{P_{SS}}{P_G} \right)}$$

Improve turbine cycle performance

Station Service

Improve boiler efficiency

Reduce auxiliary power

Thermal drying of high-moisture coals has a positive effect on boiler efficiency, station service and turbine cycle performance.

Coal Creek Station

Coal Creek Units #1 and #2...

- 2 X 600 MW Natural Circulation
- Tangentially Fired, Dual Furnace
- 8 X 8 burners, plus SOFA
- Eight Pulverizers per Unit
- Mine Mouth, ND Lignite
 - 6,200 BTU/lb
 - 38% moisture
- Commissioned 1979, 1981
- Base Loaded
- Wet FGD's, No SCR's
- Closed Loop Cooling



Problem:

- Coal moisture has a large negative effect on boiler efficiency, station service power and unit heat rate.
- For a 600 MW lignite-fired unit, fuel moisture is responsible for:
 - 9% higher coal flow rate
 - 20 MW of station service power
 - 20% higher flue gas flow rate
 - Increased operating and maintenance cost
- Can a low-temperature waste heat be used to reduce fuel moisture?

GREAT RIVER ENERGY™



A Techedna Energy Cooperative



LEHIGH UNIVERSITY



FALKIRK THE FALKIRK MINING COMPANY



North Dakota Industrial Commission



Lignite Fuel Enhancement



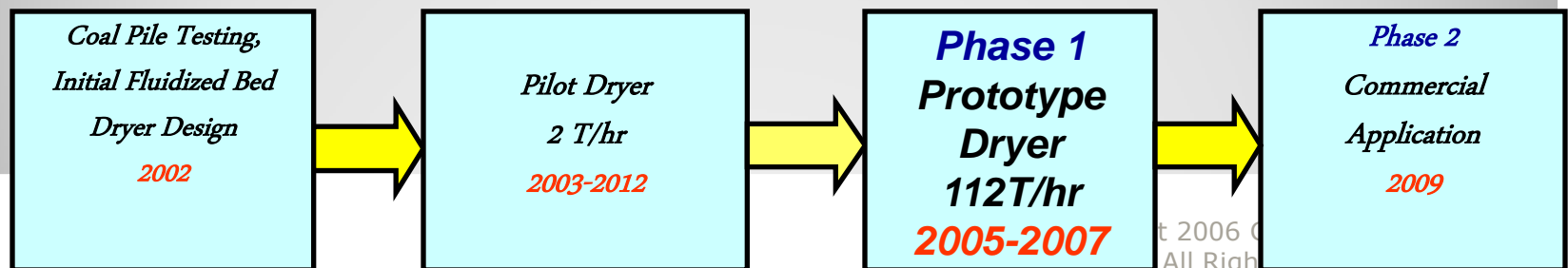
Huge Collaborative Effort

Project Goals and Schedule

- **Goals and Objectives:**

- Reduce moisture content of lignite, PRB, and other high-moisture fuels.
- Use waste heat from the power plant.
- Modify existing coal handling systems.
- Increase competitive position of lignite-, PRB-, and other high moisture coal-fired power plants.
- Reduce environmental impact of lignite-, PRB-, and other high-moisture coal-fired power plants

- **Project Phases and Schedule:**

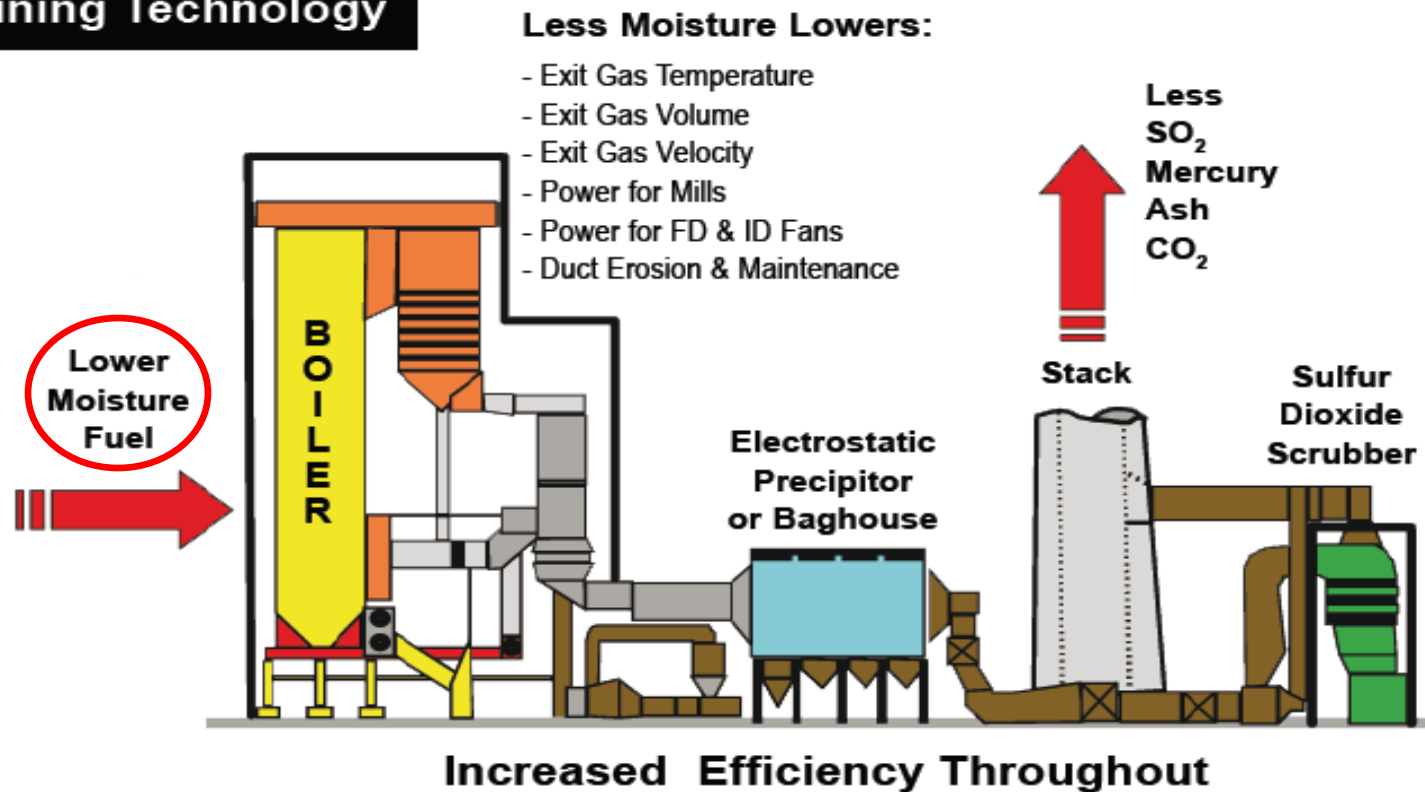


Parameter	SE Bituminous	PRB	ND Lignite	Texas Lignite
Moisture %	6.4	28.5	37.1	32.4
Ash %	6.7	5.2	11	13.3
Nitrogen %	1.4	0.7	0.5	0.8
Sulfur %	1.6	0.5	0.7	1.33
HHV Btu/lb	13,387	8,740	6,310	6,840
Ash Softening °F	2,714	2,160	2,150	N/A

Properties of Low Rank Coals

DryFinishing™ process impacts

DryFinishing Technology



Effect of Coal Moisture on Plant Equipment

- **Mills**

- Lower coal flow rate and moisture content → Lower mill power
- Fewer mills need to be in service → Flexibility in mill maintenance

- **Fans**

- Lower flue gas and air flow rates, lower drafts → Lower fan power

- **Air Preheaters**

- Lower drafts → Lower ΔP s → Lower APH leakage

- **Coal Handling Equipment**

- Less coal to handle → Lower maintenance and power requirements

- **Coal Pipes**

- Lower coal and PA flows → Lower erosion and maintenance

- **Emissions Control Equipment**

- Lower flue gas flow → Longer residence time → Better performance

- **Cooling Tower**

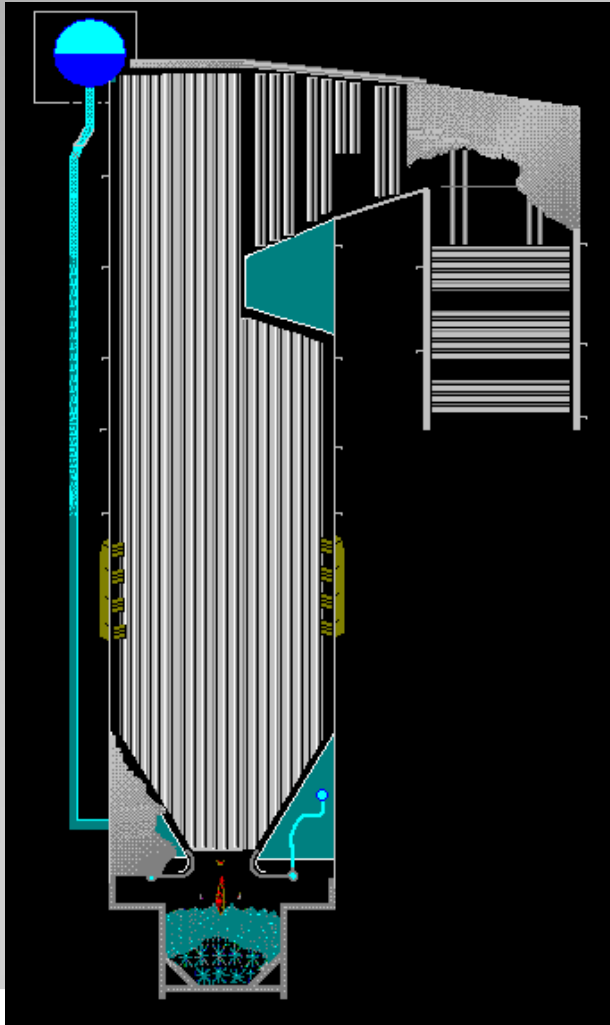
- **Turbine**

- **Plant Availability**

- Lower and more flexible maintenance → Higher plant availability

Positive, the magnitude depends on system integration

Effects of Dried Coal on Boiler



- **Boiler**

- Reduce PA/SA ratio
- Reduce total combustion air flow
- Reduce superheat sprays
- Enhance NO_x control
- Reduce ash loading
- Increase ash fusion temperature.

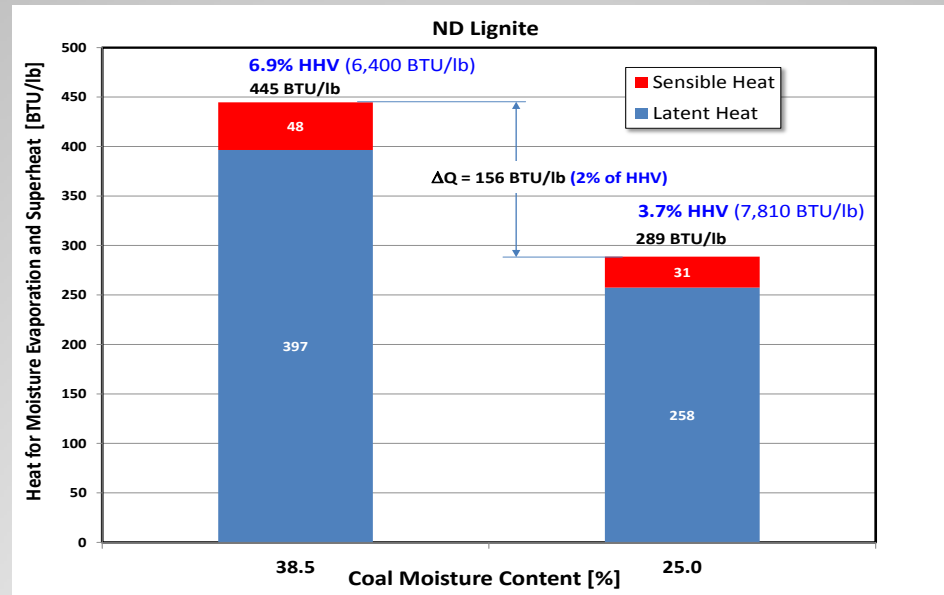
- **Air Preheater**

- Reduced ΔP
- Reduced Leakage
- Reduced maintenance

$$X_{ratio} = \frac{C_{p,air} \times \dot{M}_{air}}{C_{p,flue\ gas} \times \dot{M}_{flue\ gas}}$$

Coal Moisture effects furnace heat release

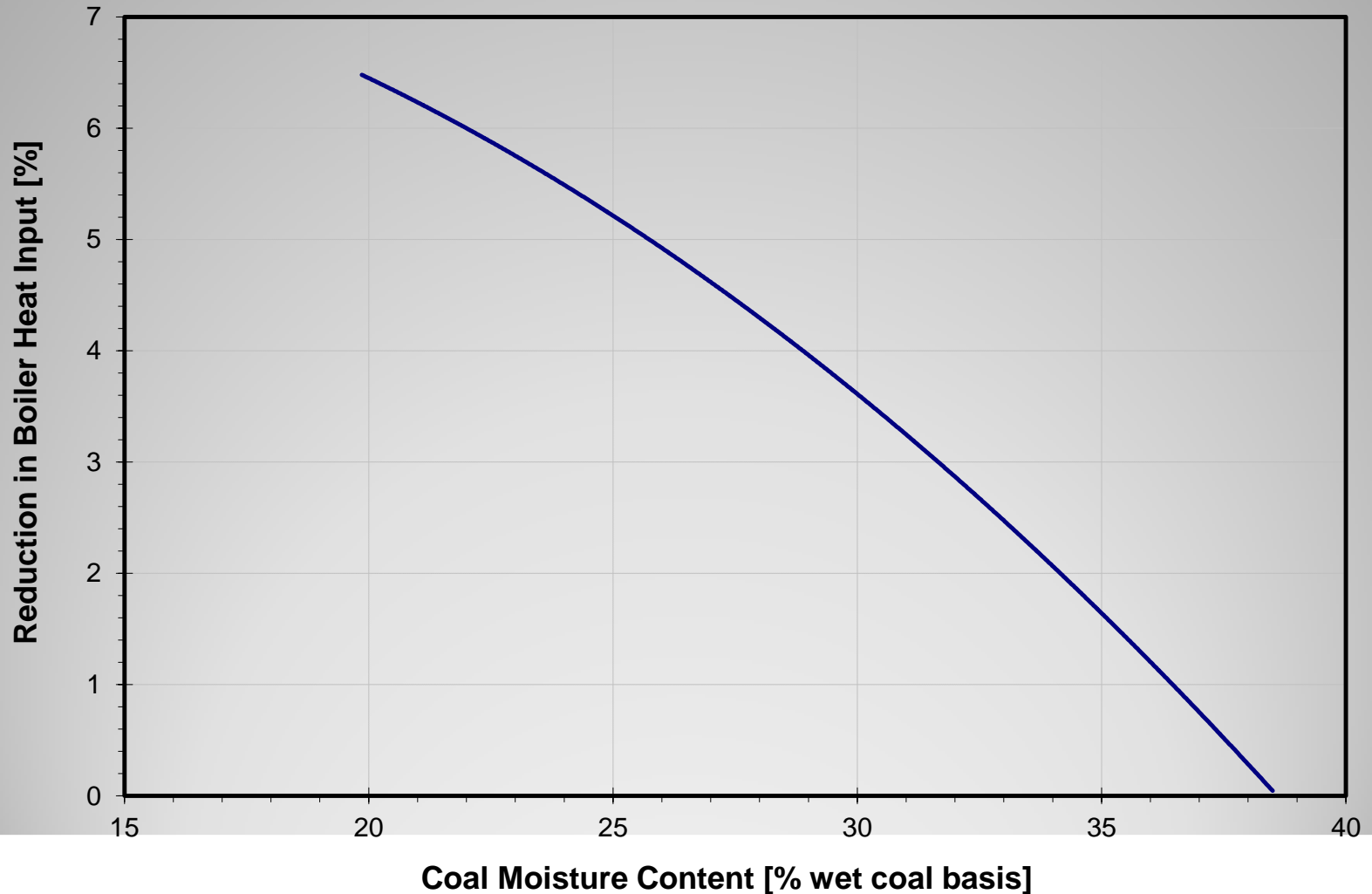
- When coal is combusted in the boiler furnace, part of the chemical energy stored in the coal is used to evaporate coal moisture



- The reduction in heat required for moisture evaporation results in increased heat release in the furnace and increased evaporation.
- For constant boiler evaporation rate (boiler thermal duty), the reduction in thermal energy required for evaporation of coal moisture results in **lower heat input** to the boiler and higher boiler efficiency.

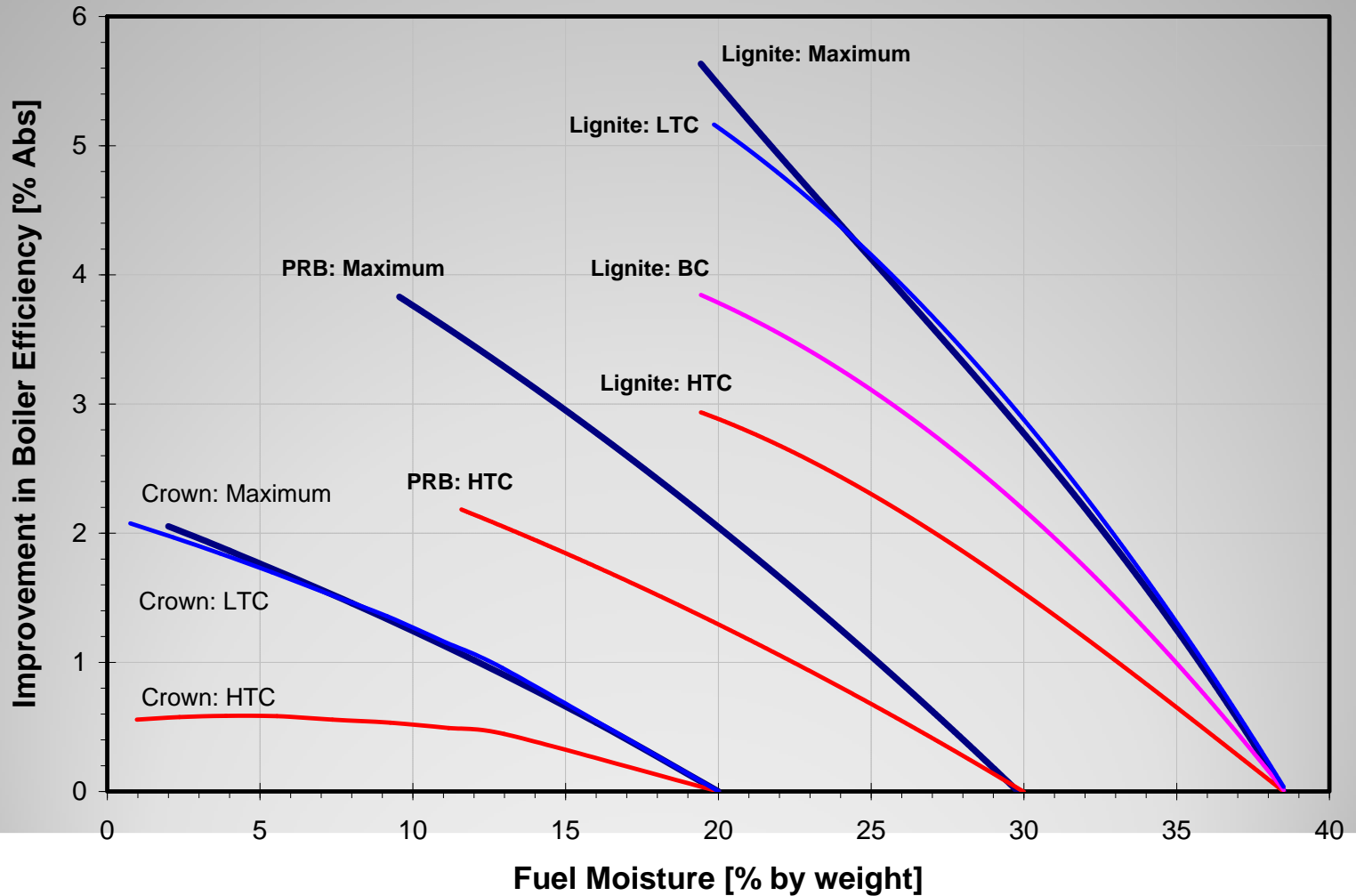
Effect of Coal Moisture on Boiler Heat Input

Effect of DryFining™ on Boiler Heat Input



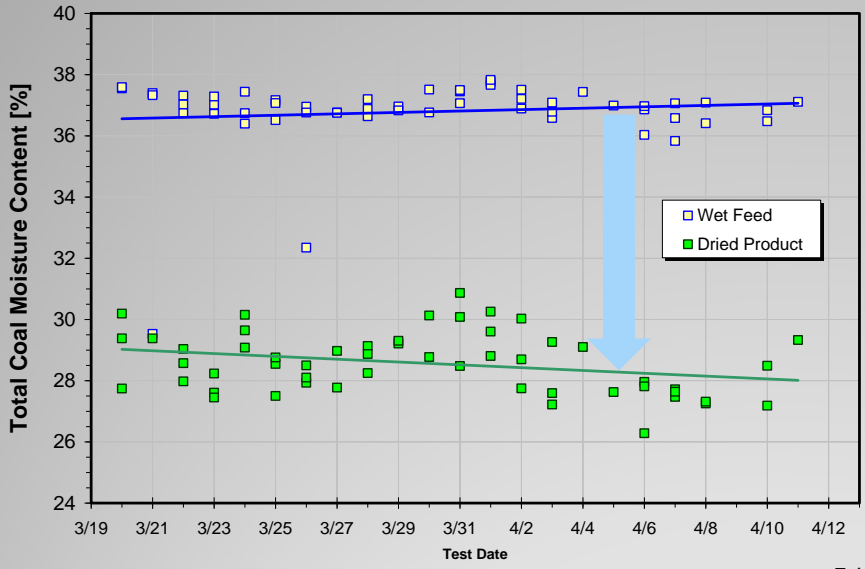
Effect of Coal Moisture on Boiler Efficiency

580 MW Unit, Lignite, PRB, and Washed Illinois Coals

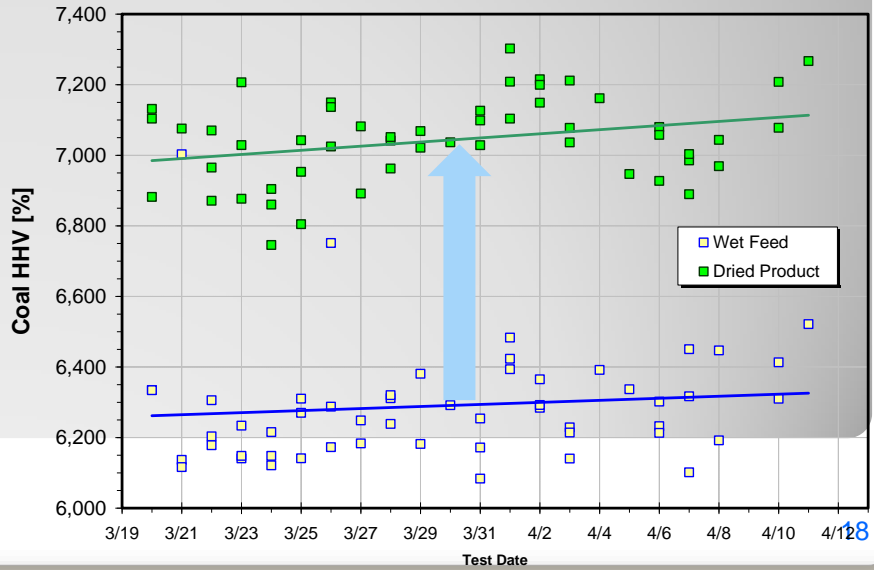


Reduced moisture, increased HHV

Prototype Coal Dryer Performance: March to April, 2006

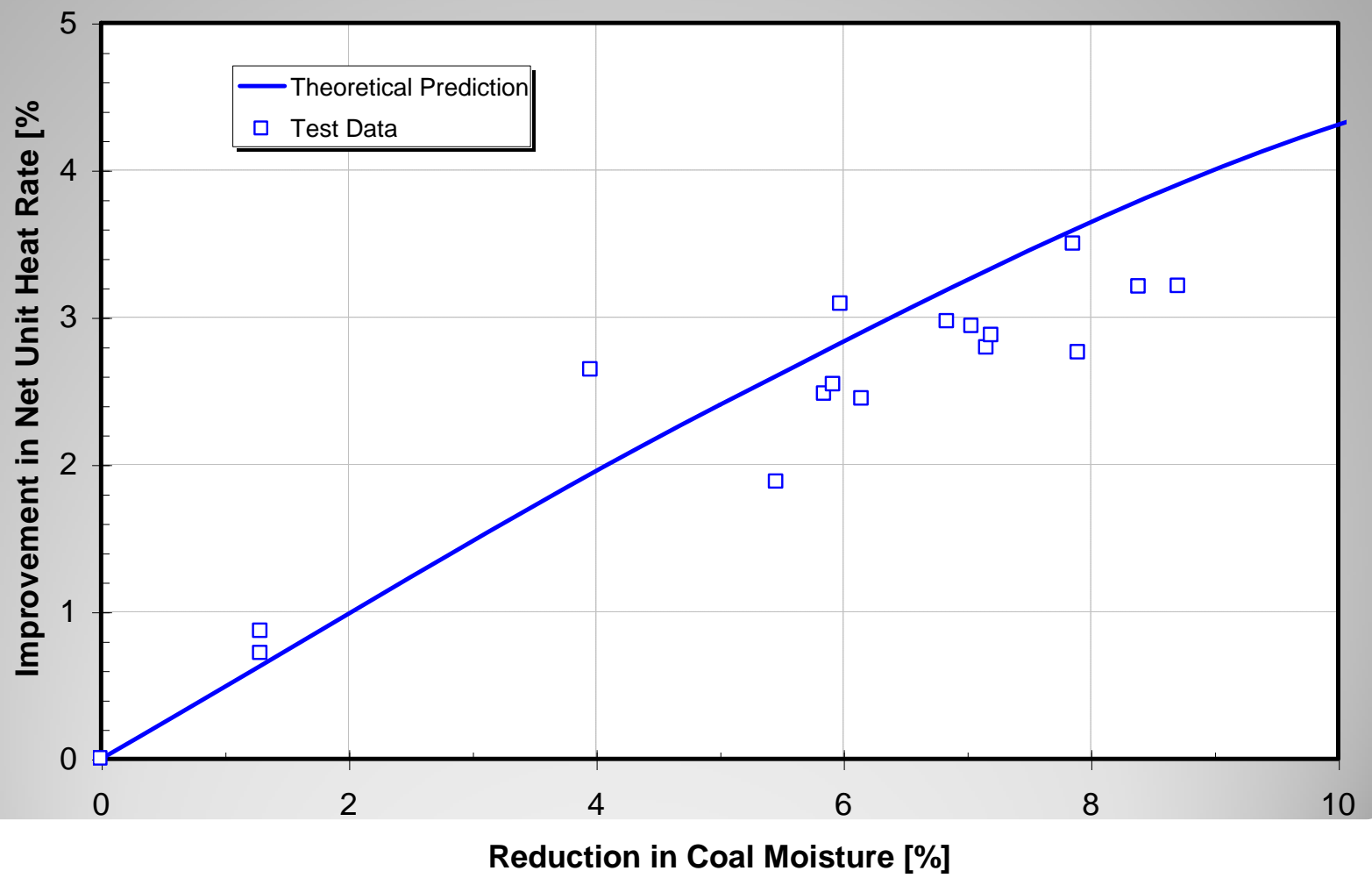


Prototype Coal Dryer Performance: March to April, 2006



Improvement in coal HHV

Reduction in coal moisture improves NHRT

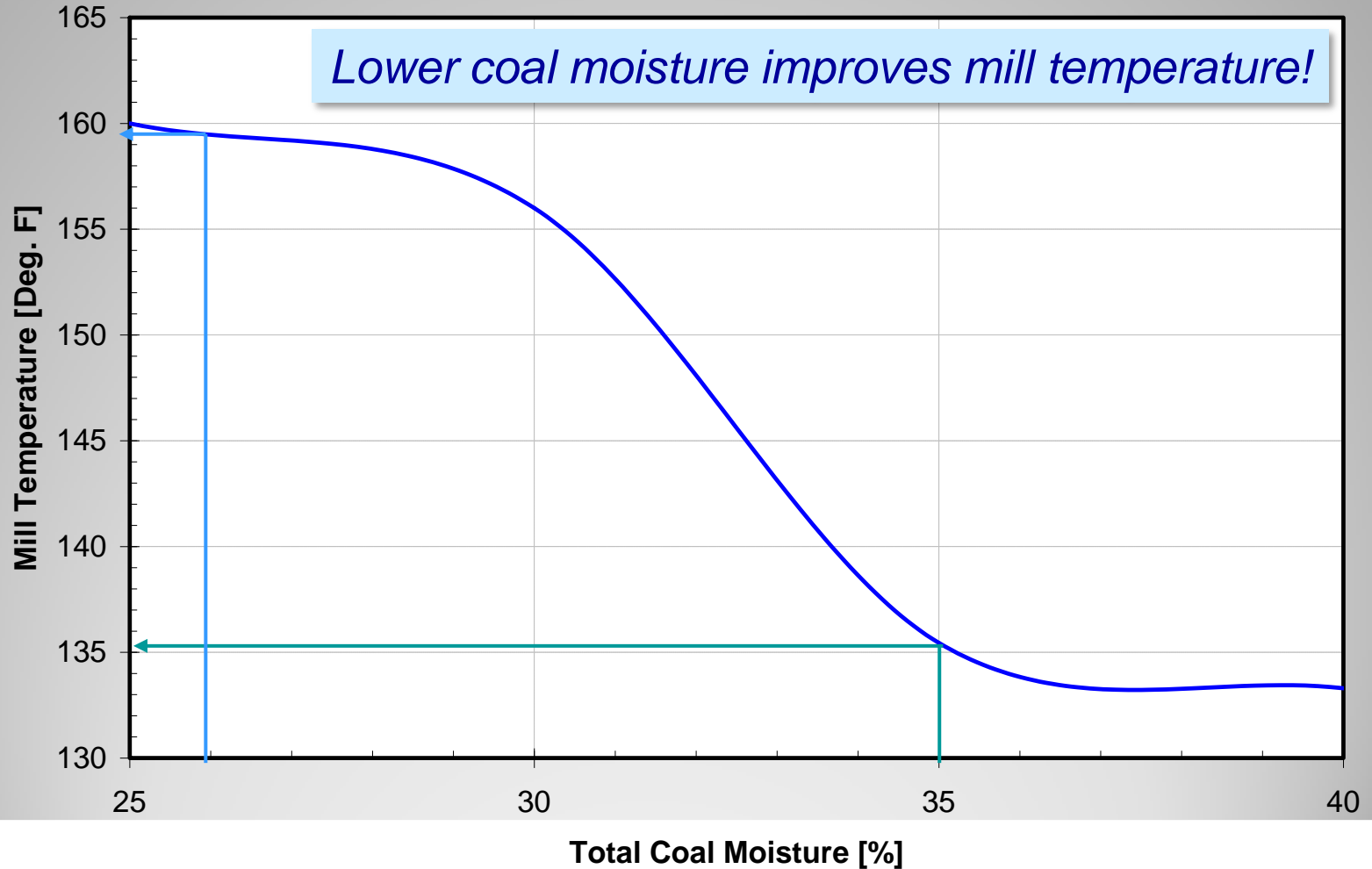


Coal Drying effects on Mills

- Reduces total coal flow, and number mills
- Reduces primary air flow requirements
- Reduces mill wear
- Reduces total mill power
- Increases mill capacity
- Coal cleaning further reduces mill wear and power
 - Pyrites, stones, rocks, etc. are removed in coal dryer

Effect of Coal Moisture on Mill Temperature

600 MW Unit

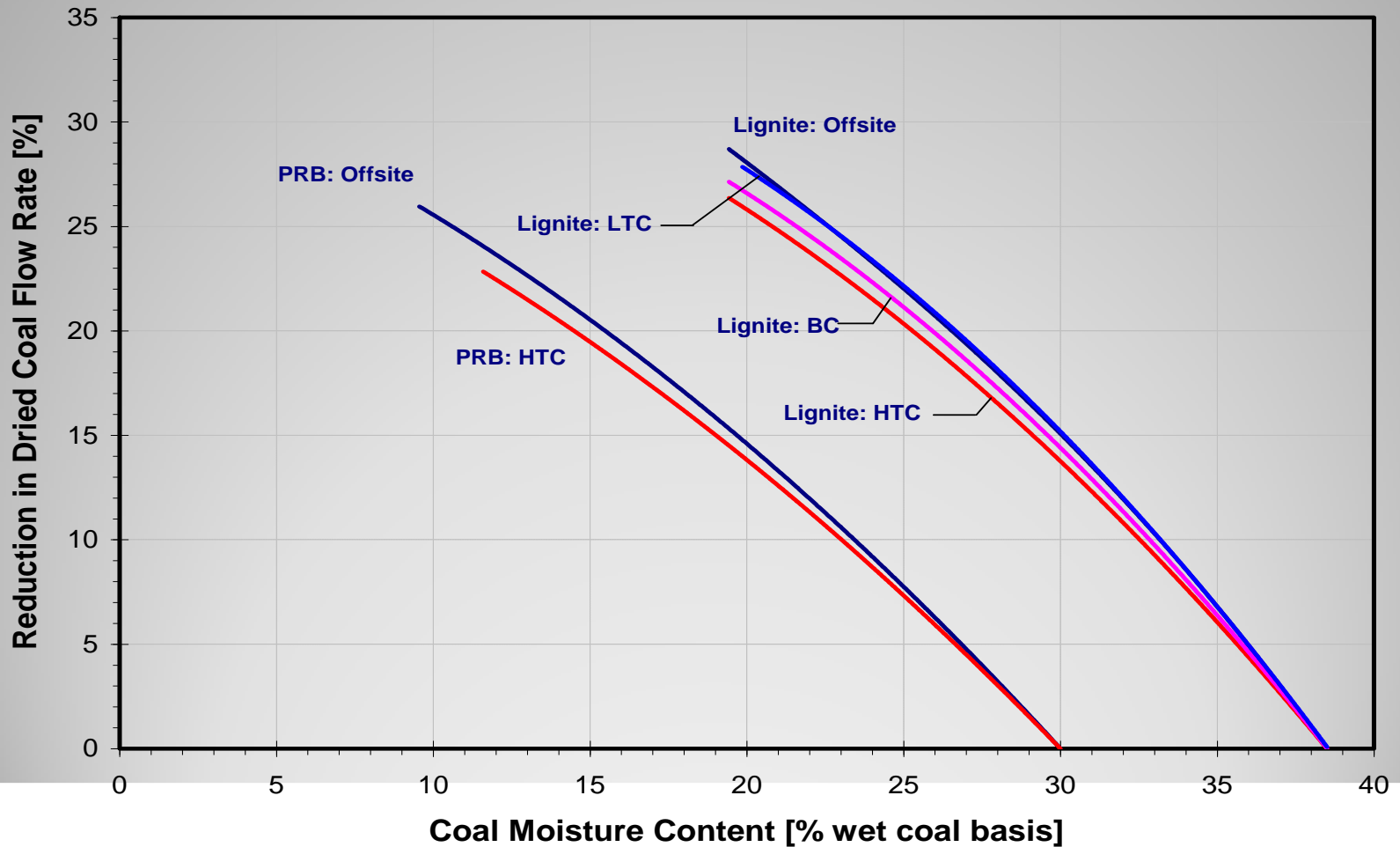


Coal Moisture effects Coal Handling

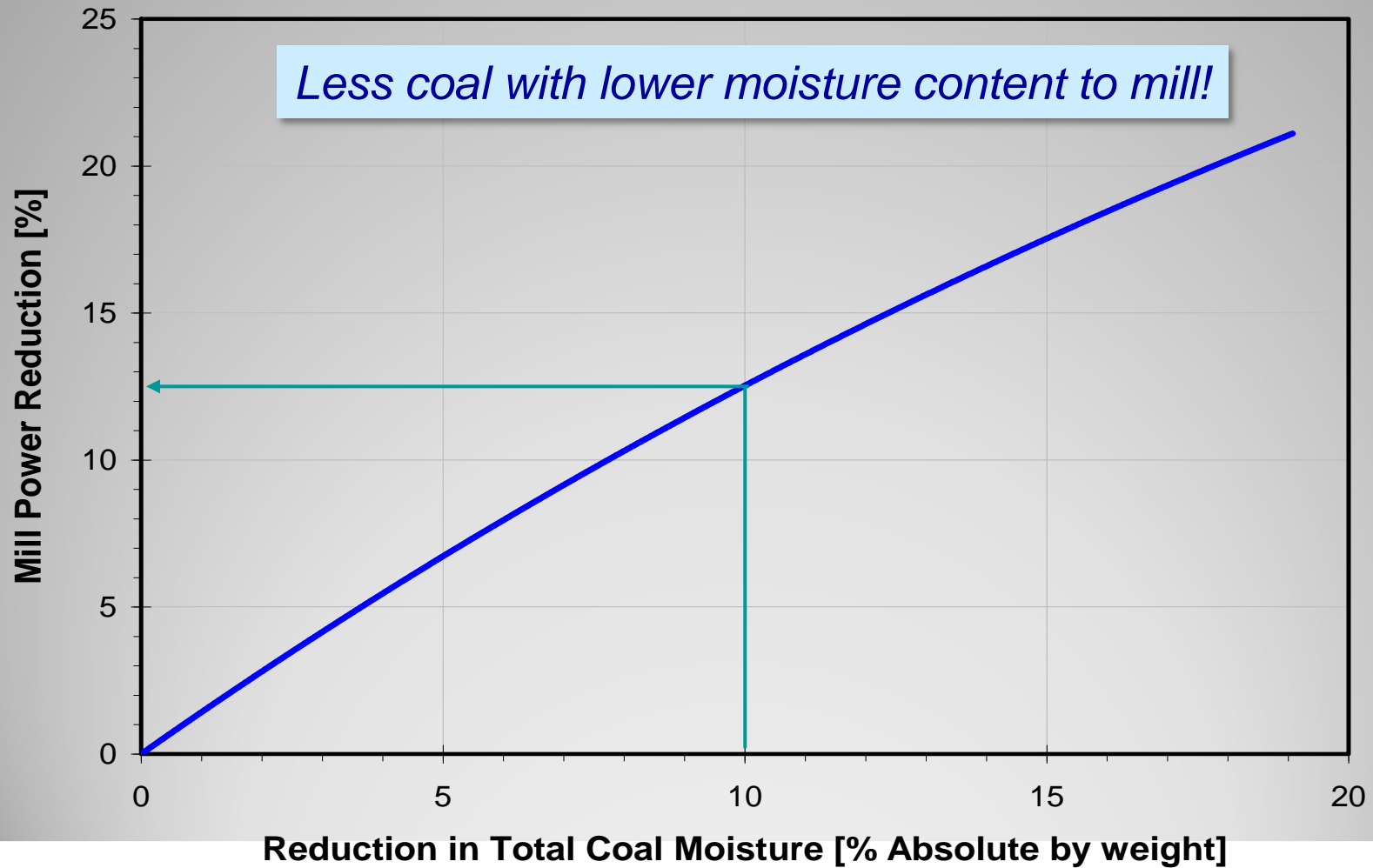
- Reduced coal flow into plant
- Fewer feeder stalls
- Improves coal energy stored in a bunker
- Spontaneous combustion (auto-ignition)?
 - Air leakage into the coal bunker (silo) must be eliminated.
 - Equilibrium coal moisture important
- Increased dust
- Improved coal flow through chutes

Coal Moisture effects Coal Flow Rate

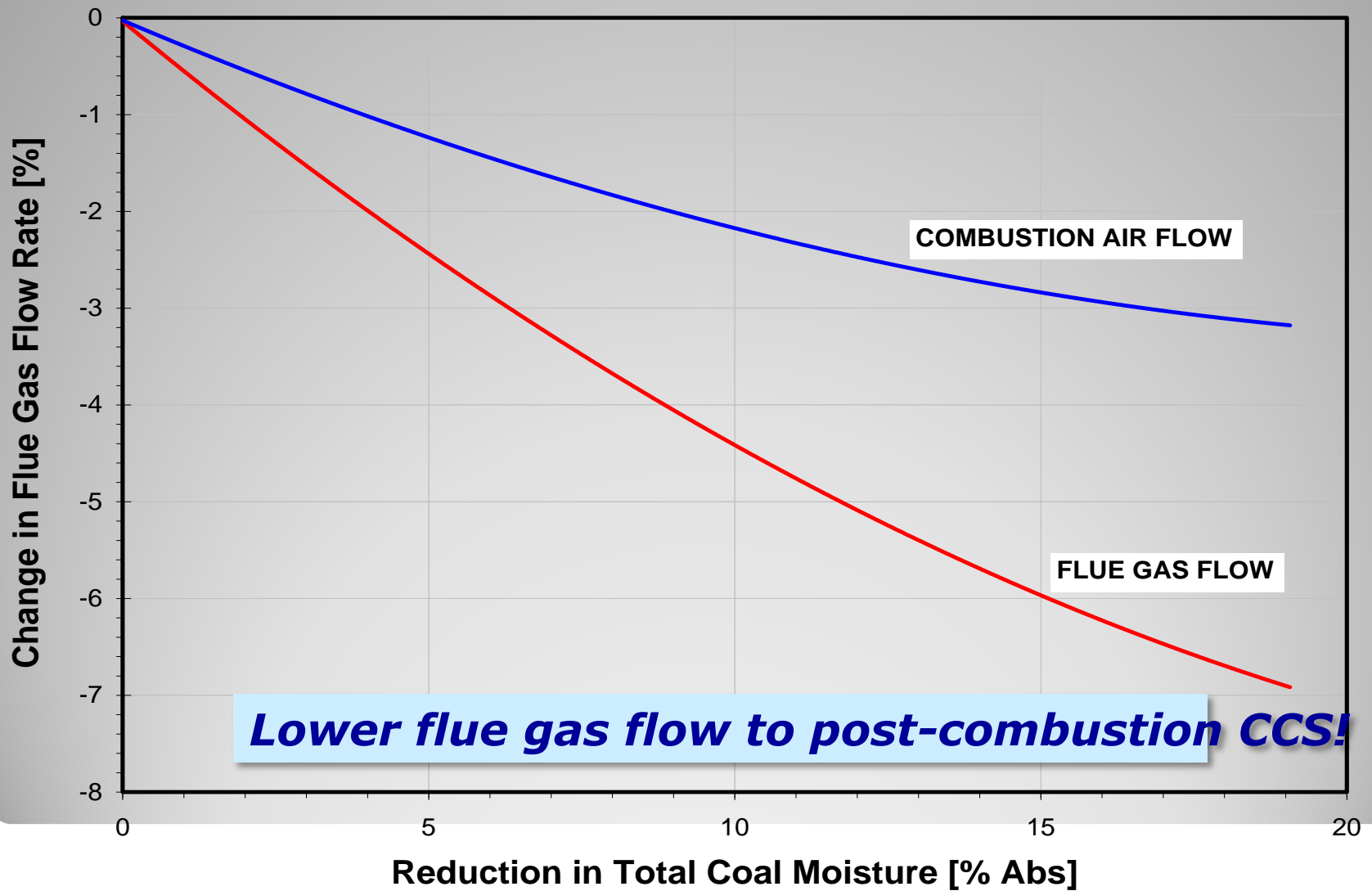
Less coal to handle and mill!



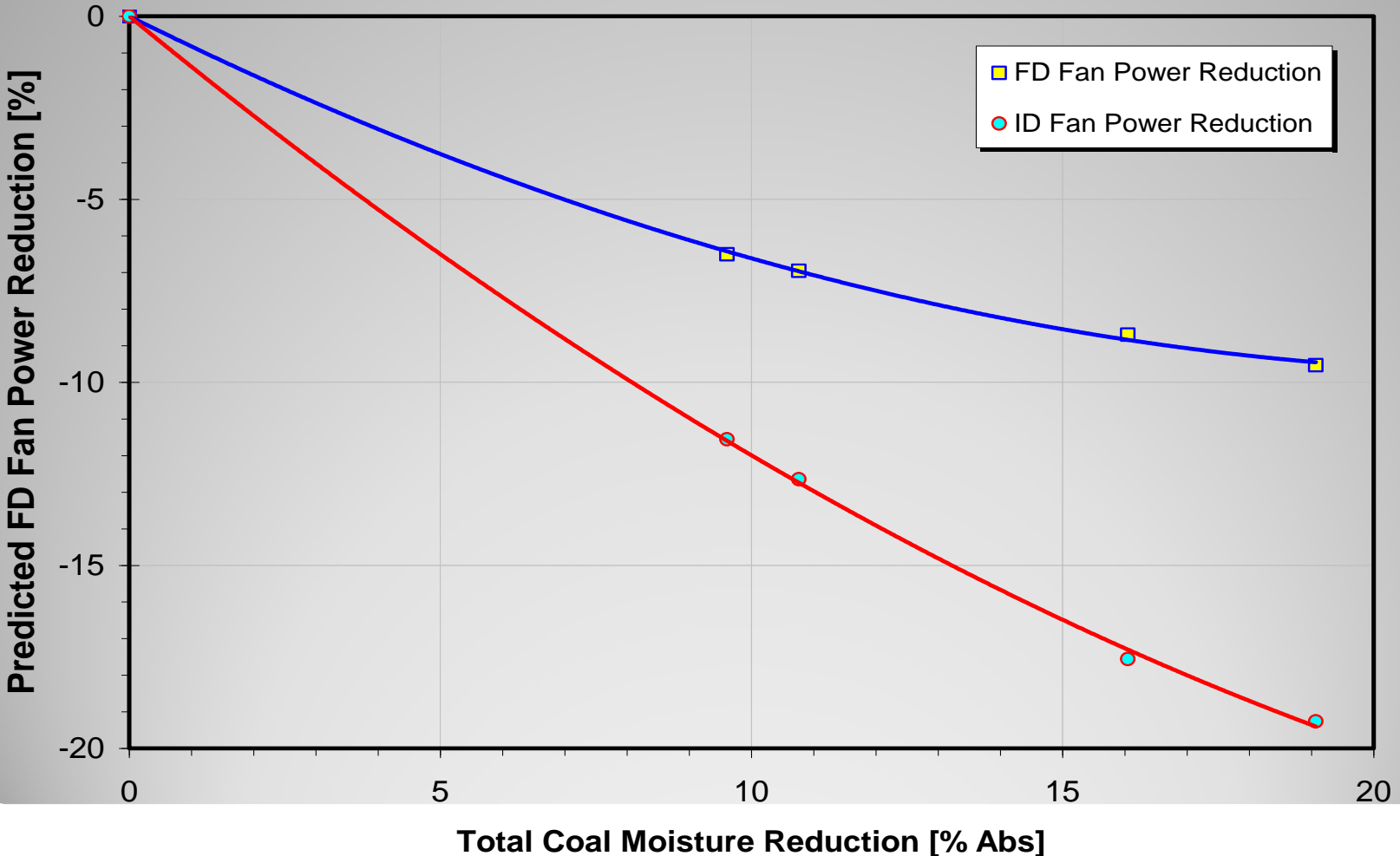
Effect of Coal Moisture on Mill Power



Effect of Coal Moisture on Flow Rates of Combustion Air and Flue Gas

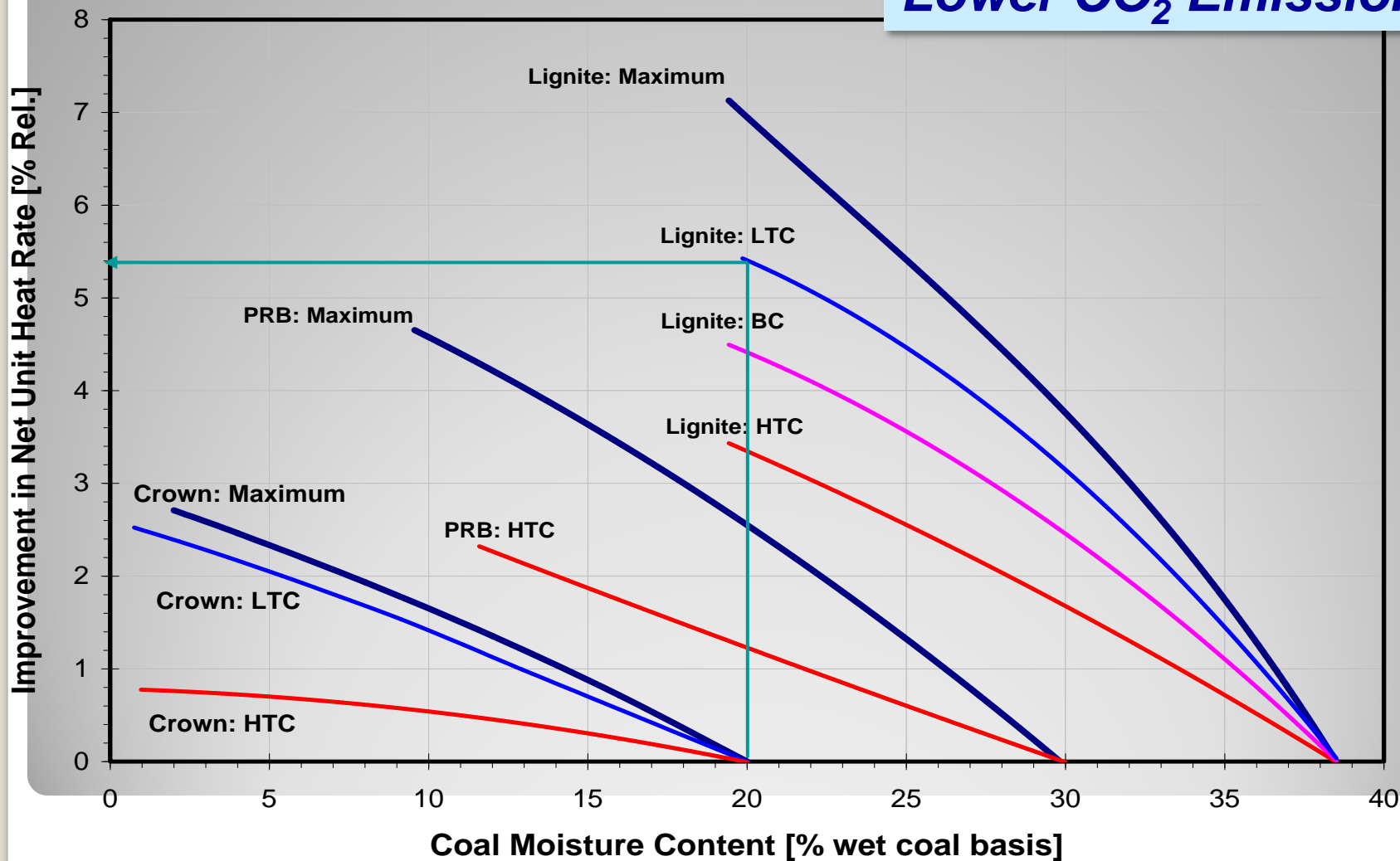


Lower coal moisture reduces fan power



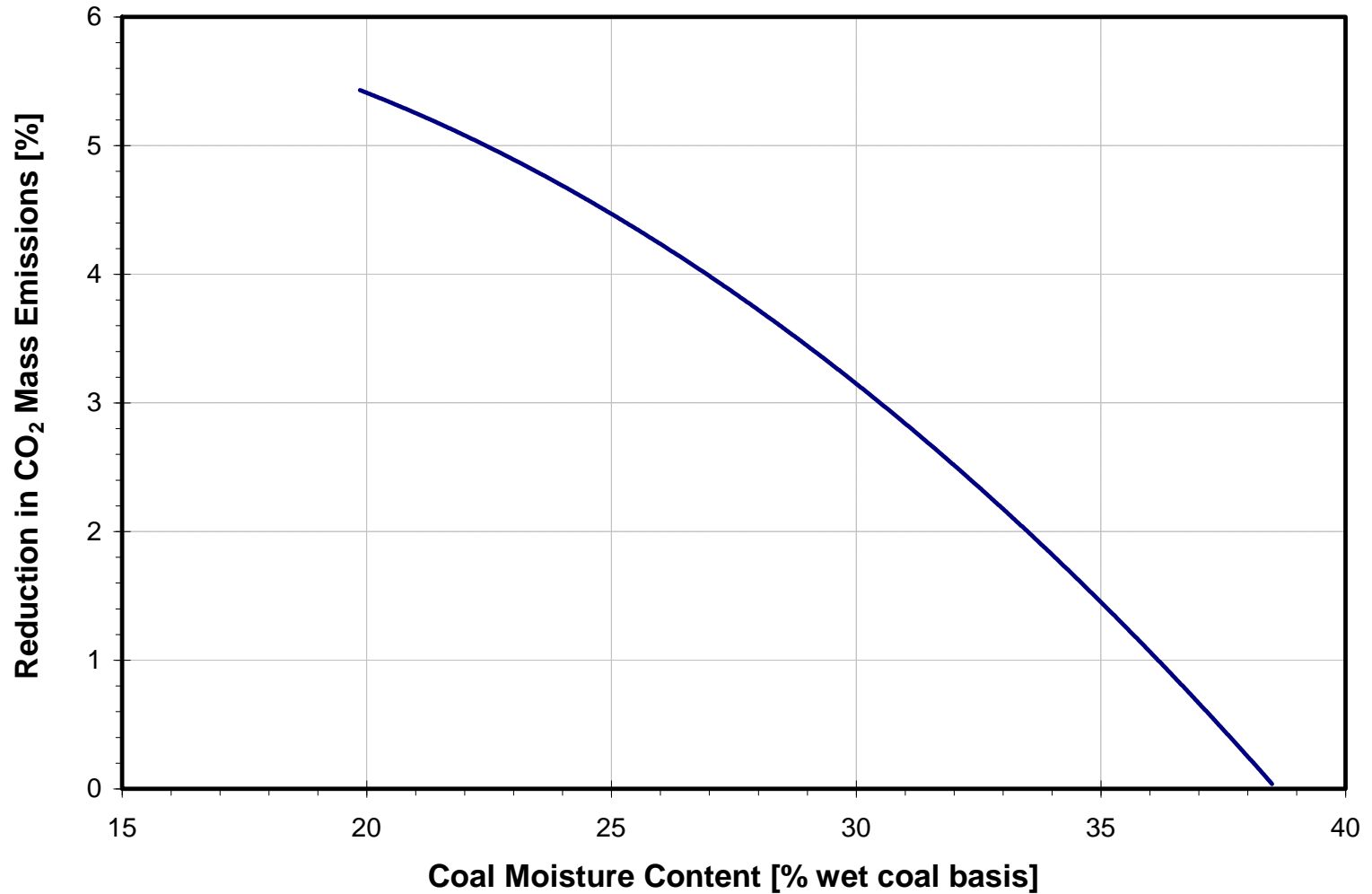
Effect of Coal Moisture and Thermal Integration of a Coal Drying System on Unit Heat Rate

Lower CO₂ Emissions!



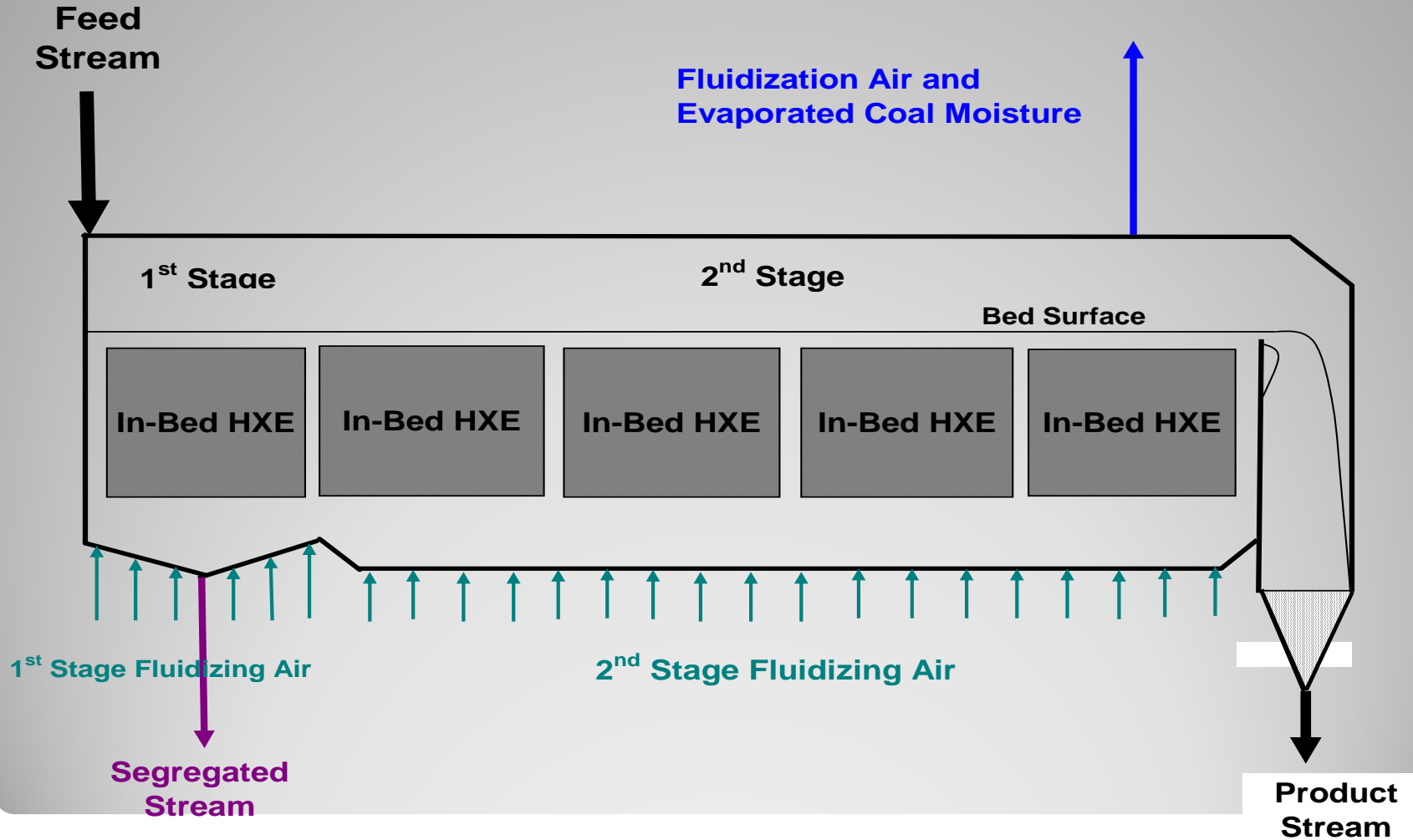
Lower coal moisture reduces CO₂ emissions

Effect of Coal Drying on CO₂ Mass Emissions: Lignite



Thermal Drying of High-Moisture Coals

DryFinishing™: Fluidized Bed Dryer

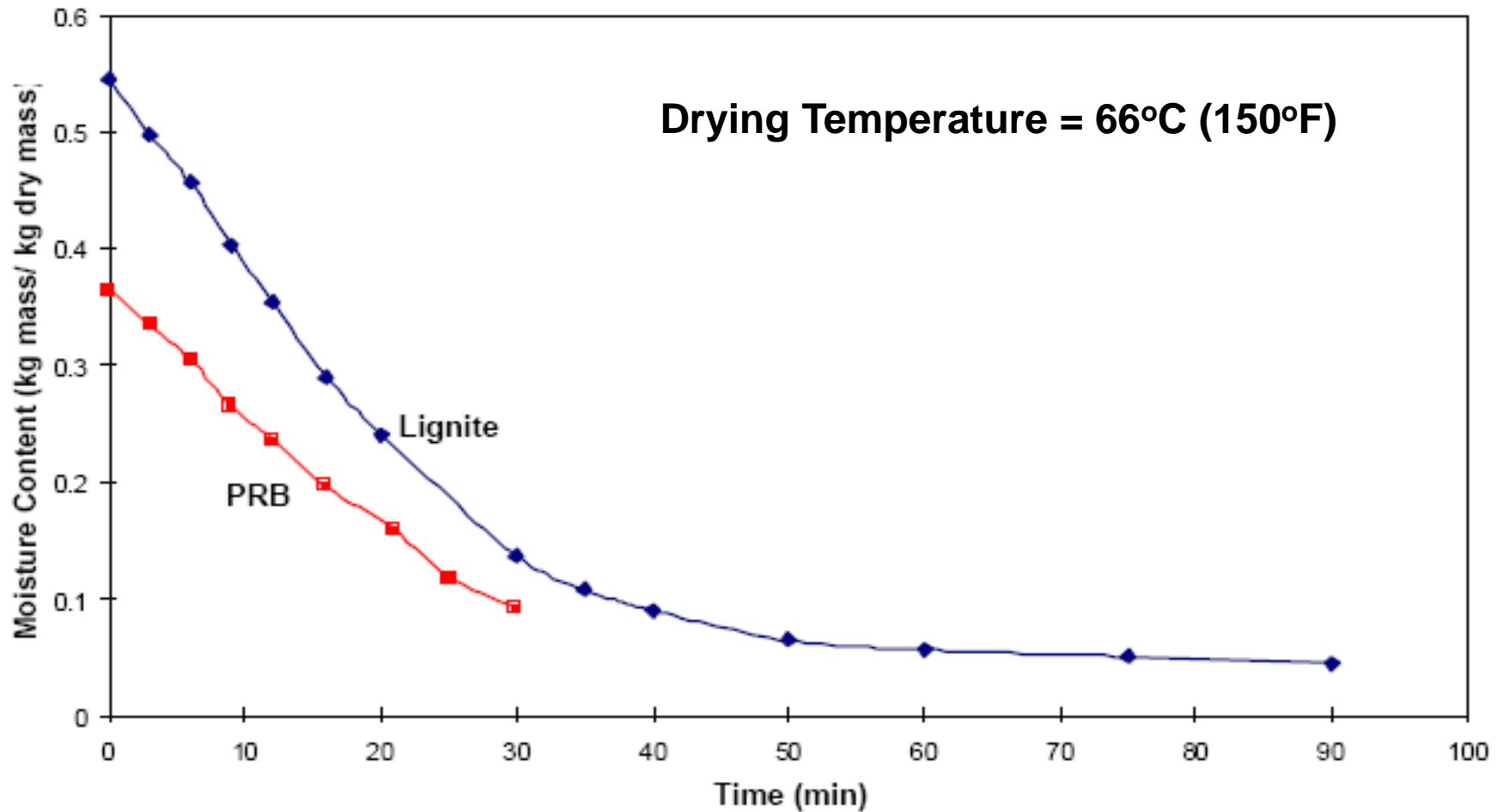


Factors Affecting Coal Drying Rate and Product Moisture

- Coal composition
 - Amount of free and inherent moisture
- Dryer residence time
- Dryer heat flux
- Temperature of fluidizing air
- Flow rate of fluidizing air
- Humidity of fluidizing air

Moisture Content vs. Residence Time

MOISTURE CONTENT VERSUS TIME

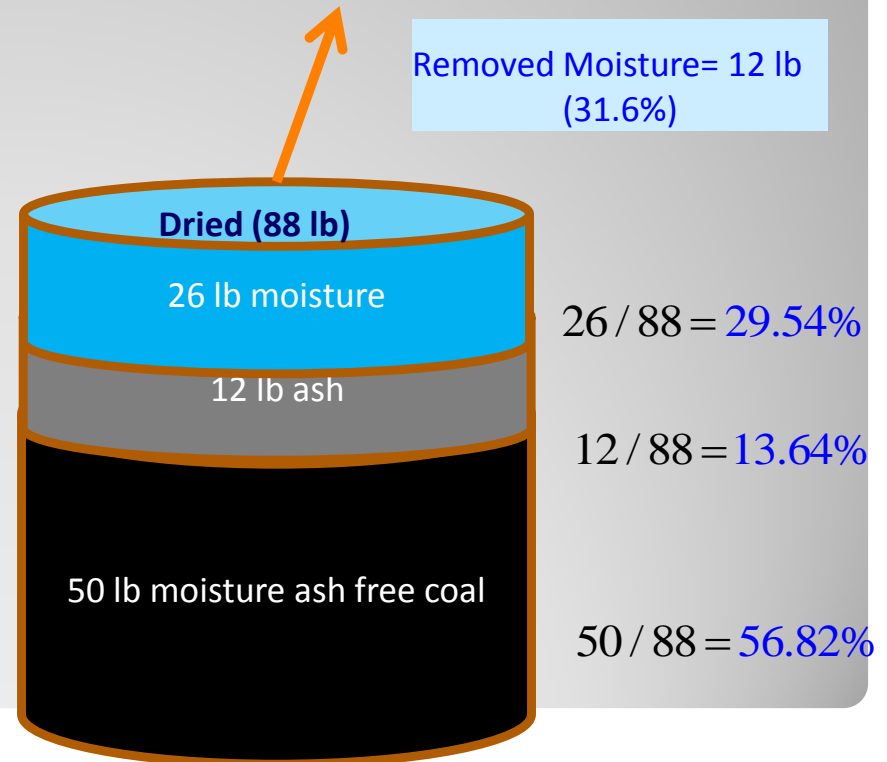
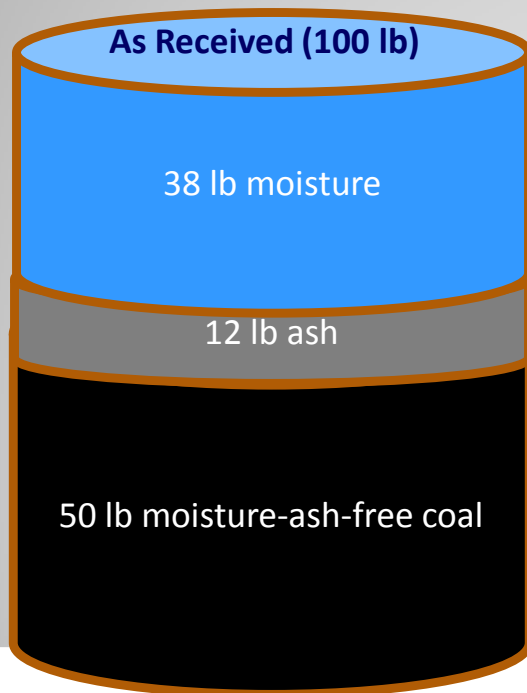


Calculating Coal Properties

$$TM = \frac{\text{lb coal moisture}}{\text{lb wet coal}}$$

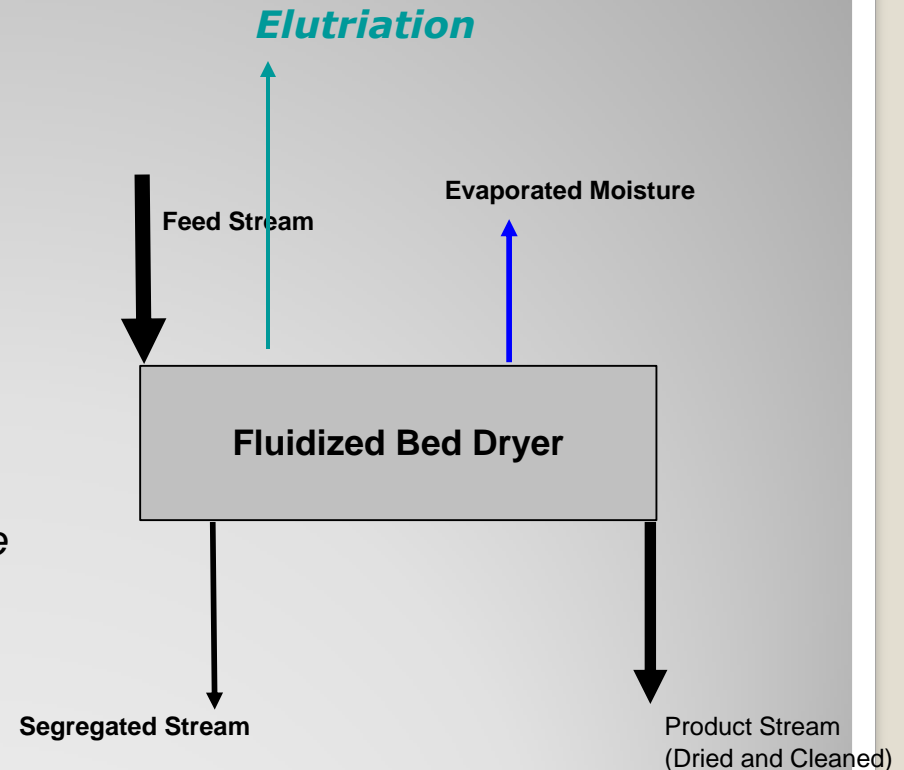
$$HHV_{Dried} = \frac{HHV_{AR}}{1 - \Delta TM_{Removed}}$$

Parameter	Units	AR	Dried
TM	%	38.0	29.5
Coal Moisture	lb/lb wet coal	0.38	0.26
Removed Moisture	lb/lb wet coal		0.12
HHV	BTU/lb	6,200	7,045
Ash	%	12	13.64

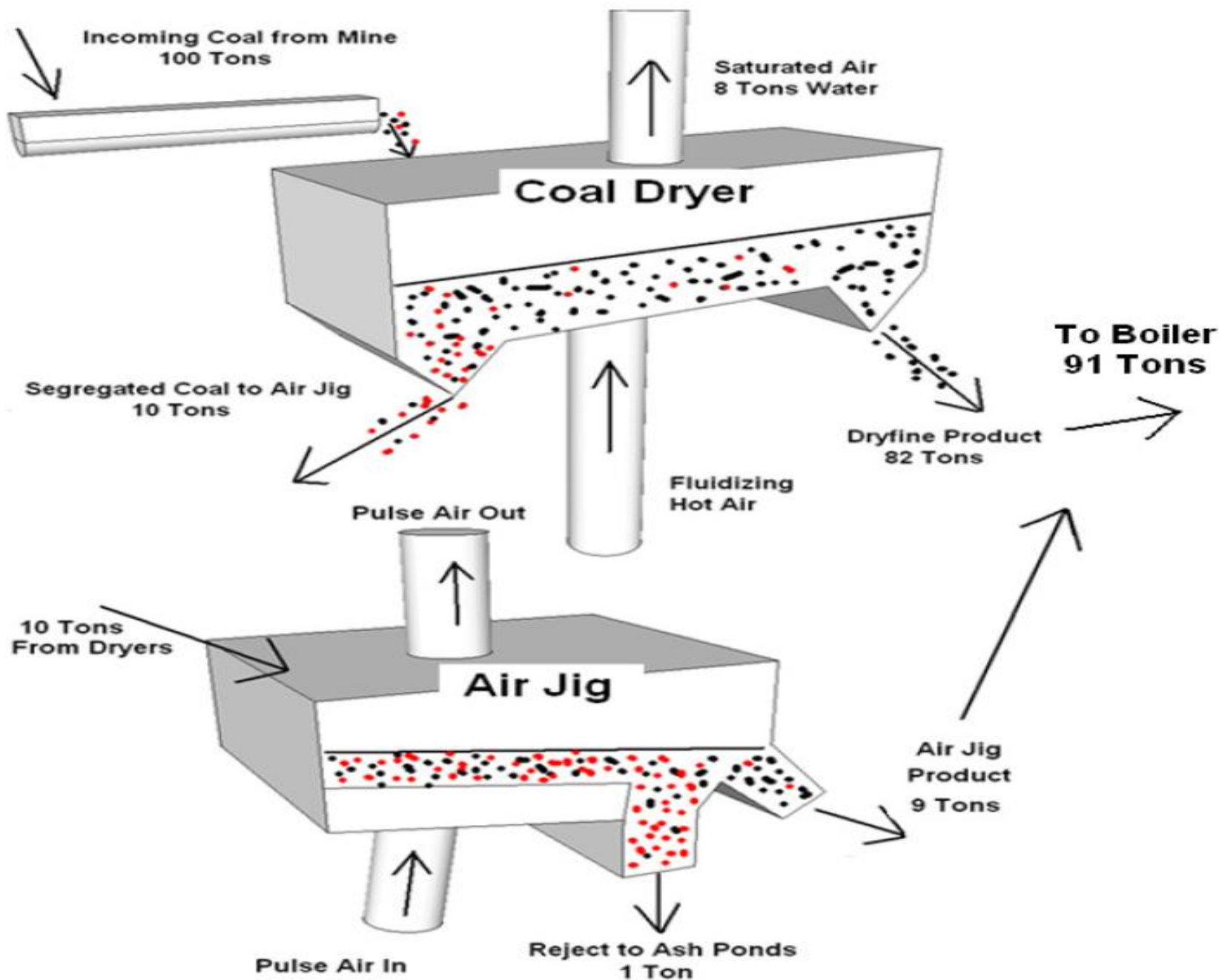


Dryer Inlet and Outlet Streams

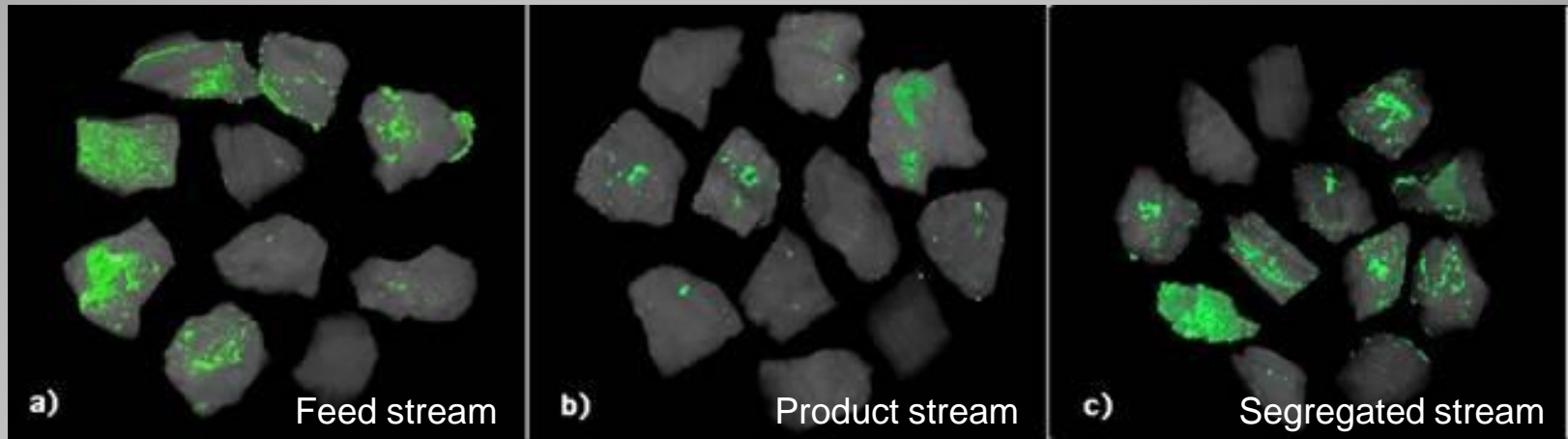
- **Raw coal feed stream**
 - High moisture
- **Elutriated fines (dust) stream**
 - Fine material
 - High ash and sulfur content
 - Low heat content
- **Segregated Stream – rejects**
 - A mixture of non-fluidizable and fluidizable materials
 - High in sulfur and mercury
 - With a properly designed discharge device it is possible to concentrate non-fluidizable material in the segregated stream.
 - Major reduction in sulfur and mercury
- **DryFine Product Stream**
 - Low moisture
 - High HHV
 - Reduced sulfur and mercury contents



DryFine System Overview



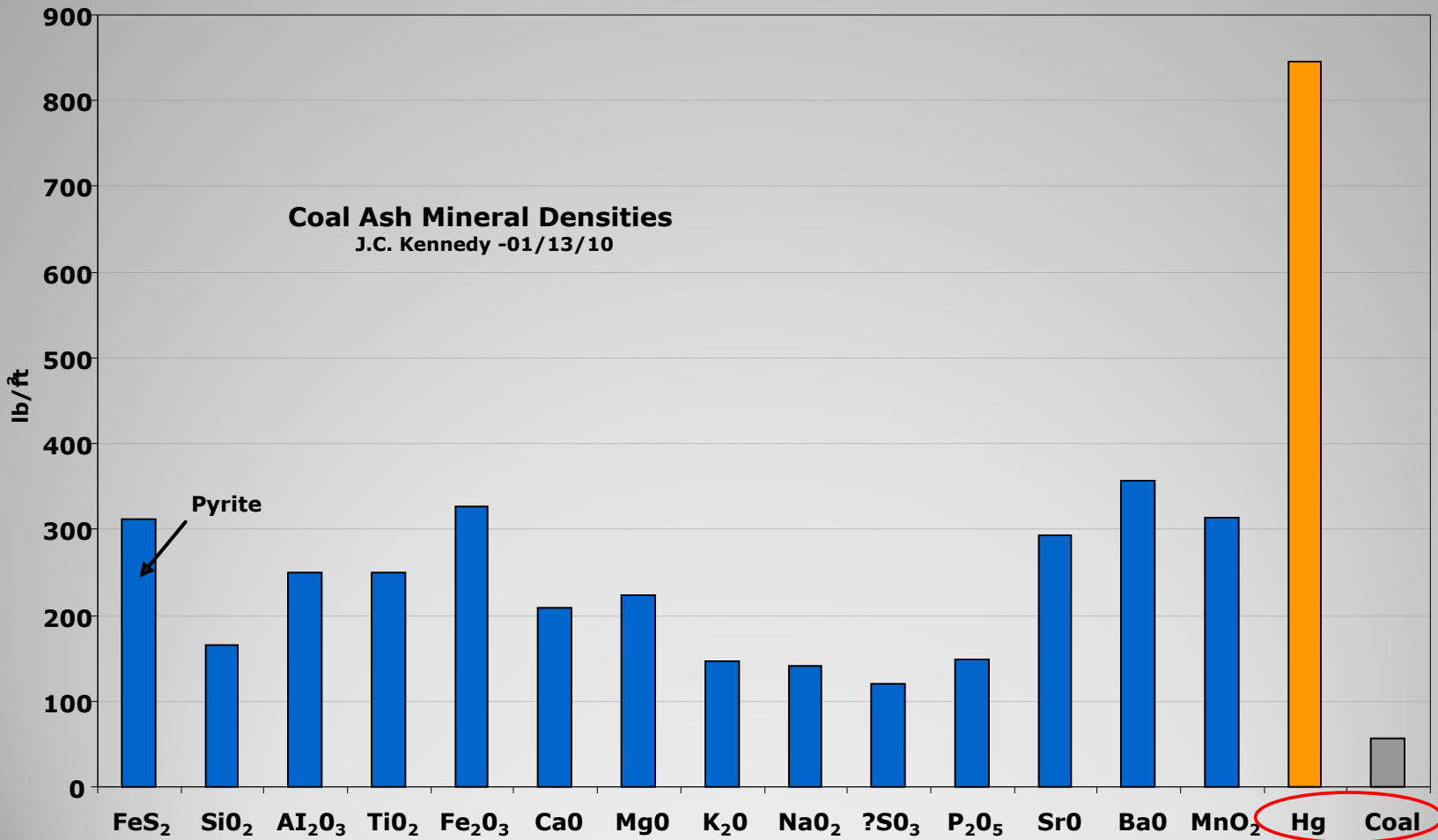
Coal morphology changes caused by drying



- Coal is shown as transparent grey, silicates and other minerals in green color.
- Based on visual observation feed and segregated streams are both relatively richer in silicates compared to the partially dried (product) stream.
- Quantitatively, feed stream contains **4.8%** of silicates (by volume), while product and segregated streams contain **2.8** and **2.7%** of silicates, respectively.
- As coal shrinks and cracks during drying the particle size distribution changes generating more surface area and exposing more of the minerals allowing for increasing mineral separation.

X-ray CT image of layers of coal from (a) feed, (b) partially dried (product), and (c) segregated streams. colored objects are higher CT absorbing material (iron and silicate containing minerals). Analysis performed at the Center for Quantitative Imaging at the Pennsylvania State University's Energy Institute.

Patented Segregation



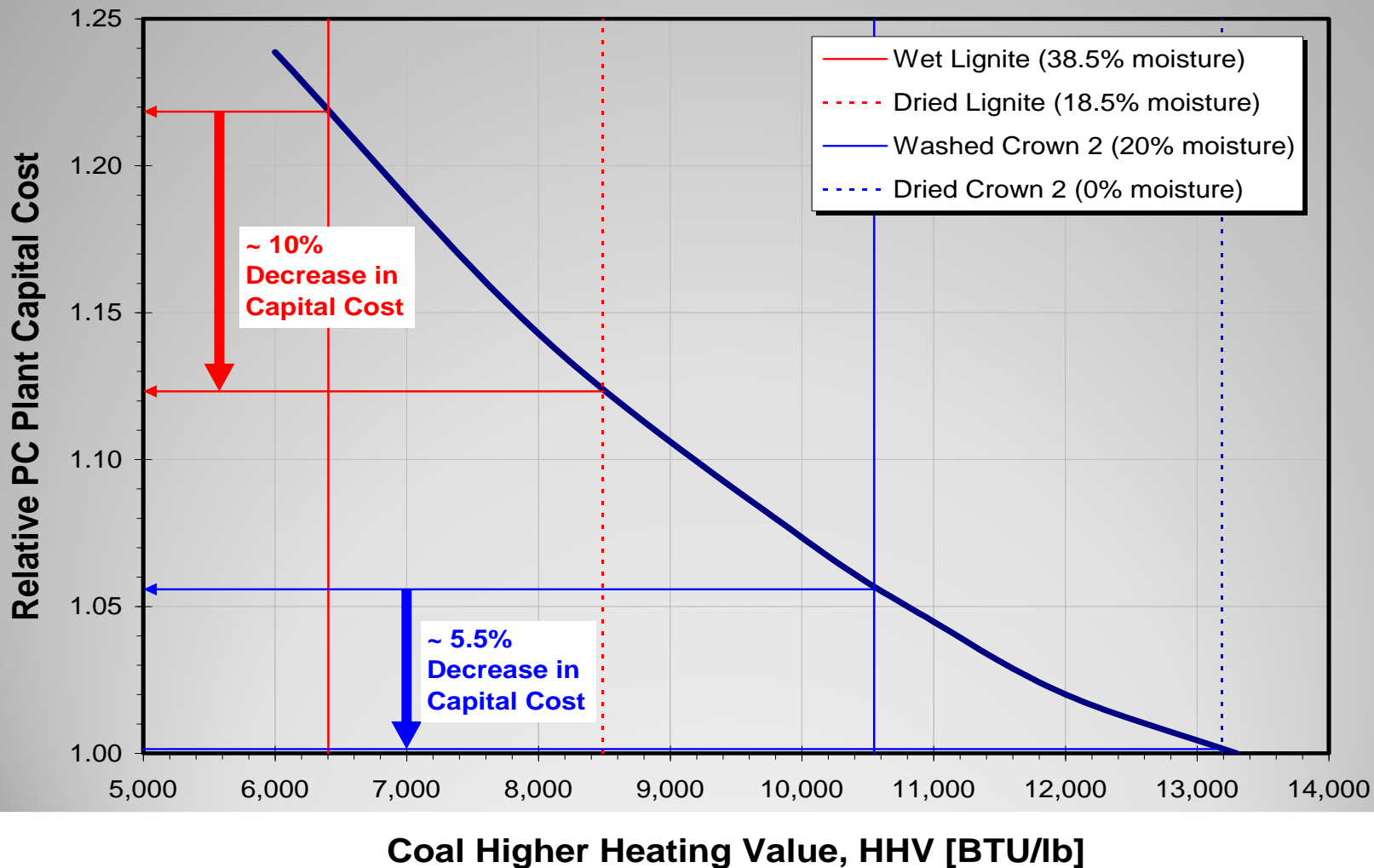
Basic characteristics of DryFining™

- Low-temperature, atmospheric pressure process
 - No high-temperature or high-pressure parts
 - No exotic materials
- Uses waste heat to remove coal moisture
 - **No external heat sources are needed**
- Simple, no moving parts
 - Equipment is simple and inexpensive to manufacture.
- Improves performance
 - Positive effect on auxiliaries
 - **Performance improvement strongly depends on system integration**
- Reduces emissions by removing **moisture**, **sulfur** and **mercury** from coal
 - Positive effect on pollution control equipment, and environmental compliance cost.

DryFining Applications

- **Retrofit** coal drying system to existing power plants firing low-rank high-moisture fuels to:
 - Improve efficiency (and recover efficiency loss due to CCS)
 - Reduce emissions & environmental compliance cost
 - Improve unit availability
 - (Alternate equipment arrangements)
- **New Design Integration** coal drying system into a new power plant design (supercritical, ultra-supercritical, gasifier-based systems, etc.) to:
 - Maximize efficiency and reduce impact of Carbon Capture
 - Reduce emissions
 - Reduce capital investment cost
 - Reduce environmental compliance cost
 - Improve unit availability
- **Coal Preparation** beneficiated coal for the market use
 - Reduce transportation costs

Lower coal moisture reduction capital cost of new power plants



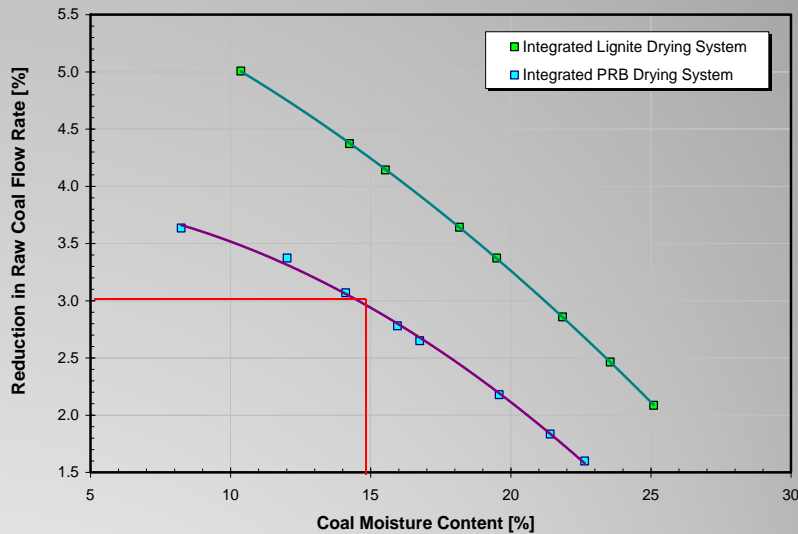
Source: EPRI

Drying at the Mine reduces transportation cost

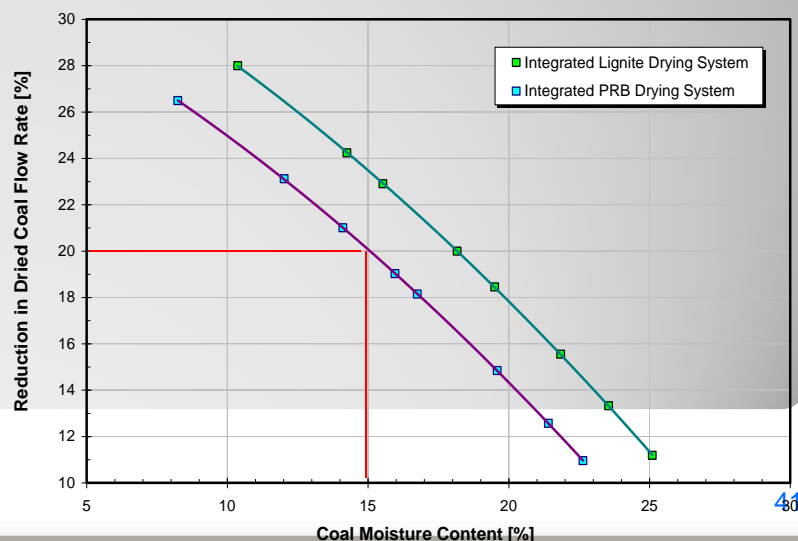
- Coal drying at the plant results in fuel saving equivalent to heat rate improvement.
- Drying at the mine results in savings equivalent to heat rate improvement plus the transportation cost of the water removed
- Example:** Buy lignite at the mine \$10/ton and ship to Plant for \$40/ton → **Total = \$50/ton**
 - Drying on site from **30%** to **15%** results in raw coal and freight saving of **3%**
 - Drying at the mine results in a **3%** reduction in raw coal and a **20%** reduction in freight, or
 - Need waste heat source at mine.

$$\frac{20\% \times \$40 + 3\% \times \$10}{\$50} = 16.7\%$$

Supercritical 650 MW Unit



Supercritical 650 MW Unit



Commercial Coal Drying System: Construction

Dryer area before & after



2015

43

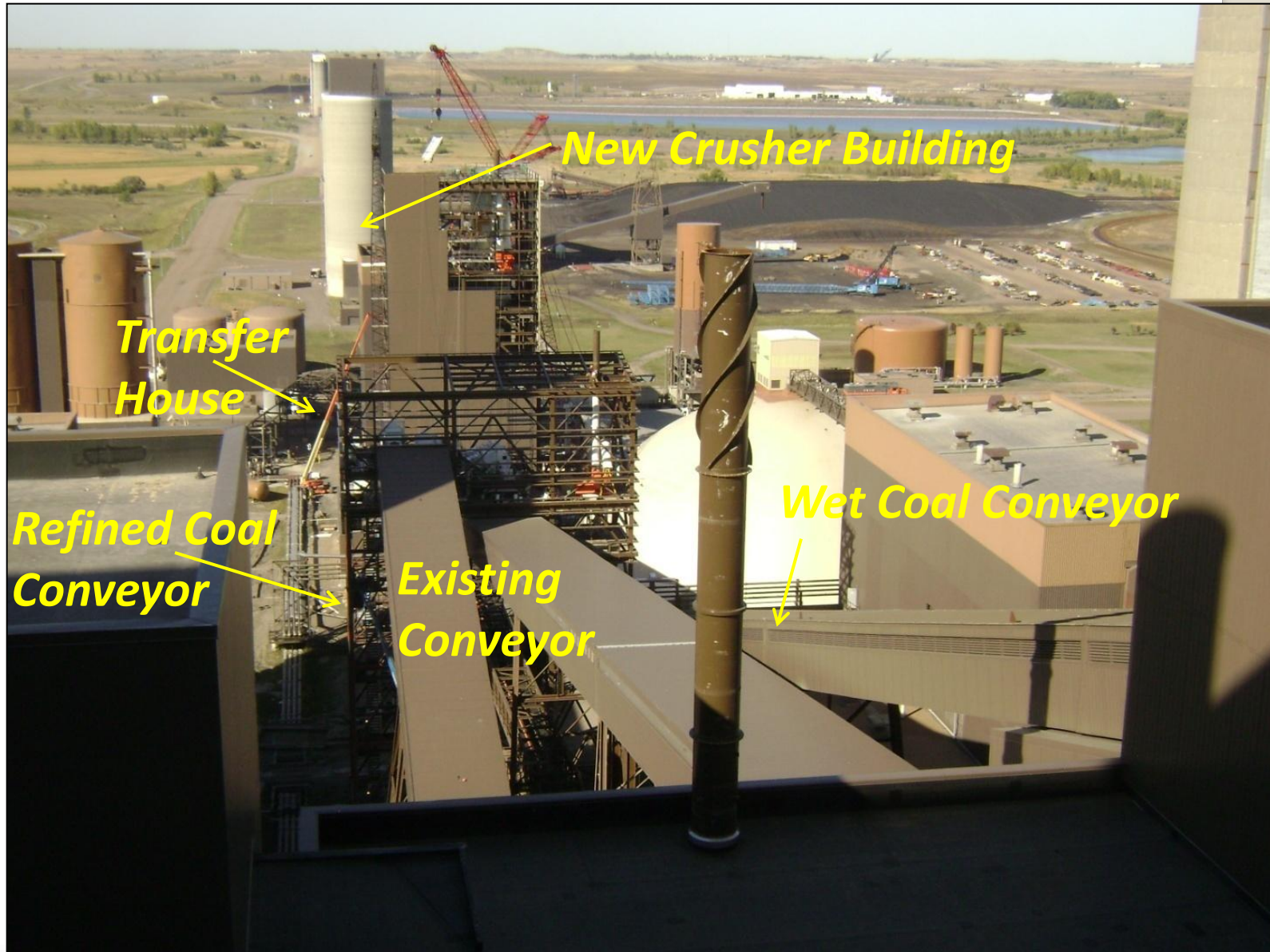
Rigging Dust Collectors



Summer 2009 Installation



DryFinishing™ conveying system



Project did not impact availability!



January 2010



CONFIDENTIAL- 48

Coal Drying System: Emissions Test Results

**(September 2009, March/April 2010,
and October 2011)**

DryFining system performance & emissions

Test	O _{2,APH,in} %	Stack flow kscfm	SO _x lb/MBtu	NO _x lb/MBtu	Hg ^T μg/Nm ³	Fuel klbs/hr
Pre	2.54	1,536	0.577	0.283	14	946
Post*	2.76	1,467	0.3055	0.194	8.75	852.5
%Diff	+8.6	-4.5	-47	-30	-37.5	-9.9

Test	Mill Power kW	HR _{net} BTU/kWh	η _B %-point	O _{2,APH,in} %	APH Leakage %	TM** %	HHV** Btu/lb
Pre	3916	10465	78.67	2.54	8.2	37.8	6,251
Post*	3544	10046	80.8	2.76	4.1	30.2	7,037
%Diff	-10.5	-4	-2.7	+8.6	-50	-20	+12.6

* Post March/April 2010 and October 2011

** Dryer functionality tests , January 2010

DryFining system performance & emissions

Test	Stack Flow klb/hr	CO _{2,Stack} % vol	CO _{2,Stack} % wt	CO ₂ Mass Emissions klb/hr	Q _{CEM} MBTU/hr	FEGT °F
Pre	6,135	13.14	19.92	1,240	5,773	2,000
Post*	5,861	13.65	20.68	1,212	5,646	2,053
%Diff	-5.1	+3.85	+3.0	-2.3	-2.2	

Test	HHV MAF BTU/lb	ID Fan Power kW	Opacity %	Burner Tilt Degrees	WFGD Inlet Temp. °F	Stack Temp. °F
Pre	12,146	8,767	6.6	19.2	345	188
Post*	12,046	7,251	5.8	11.5	309	156
%Diff	-0.8	-17.3	-0.8	-40.1	-36	-32

* Post March/April 2010 and October 2011

** Dryer functionality tests , January 2010

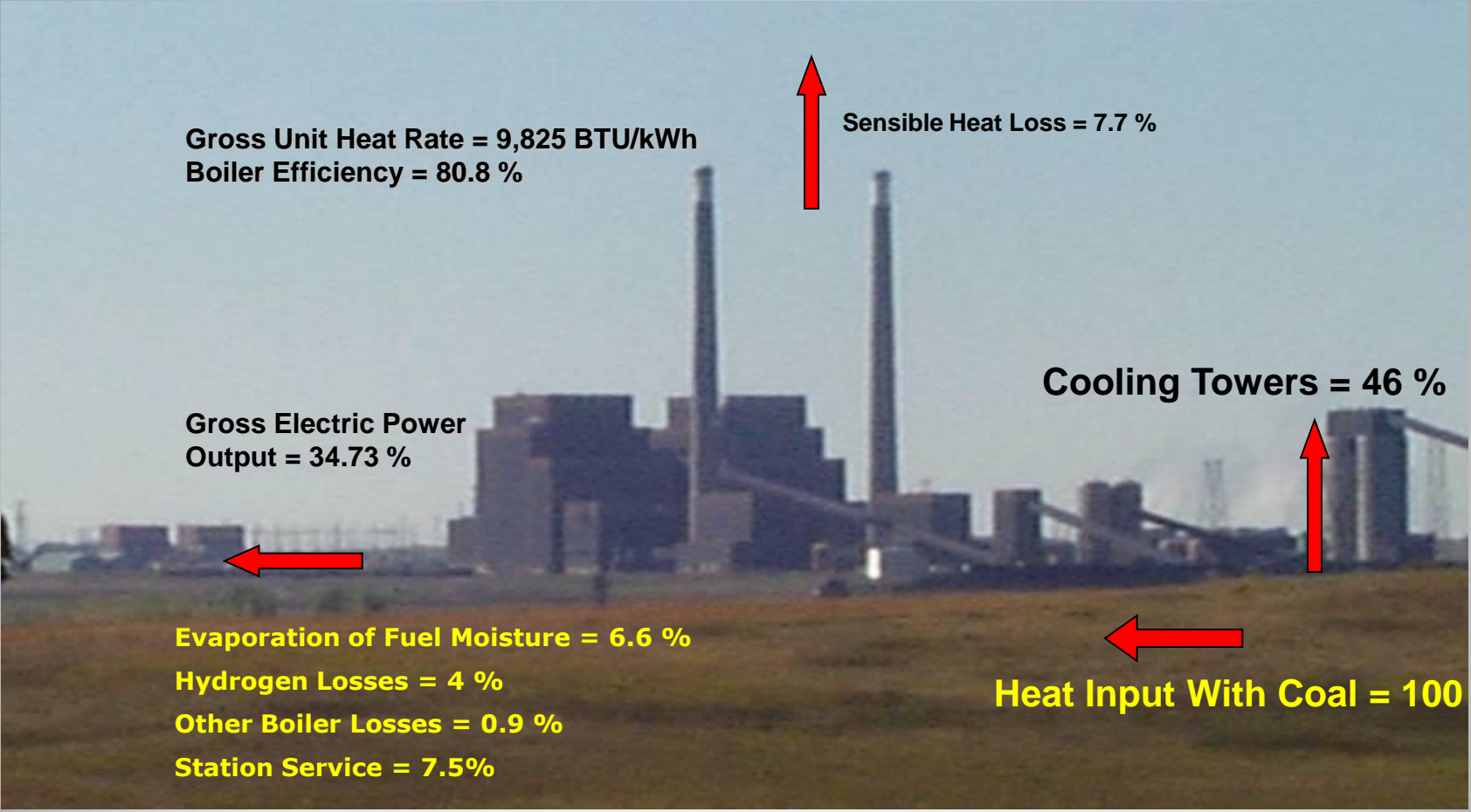
Mercury in Flue Gas

sCEM Measurements				
Measurement Location	Measured Quantity (sCEM)	Units	Wet Coal Baseline Average	Dried Coal Average
APH Inlet	Total Hg	$\mu\text{g}/\text{dNm}^3$ at 3% O_2	19.2	15.3
	Elemental Hg	$\mu\text{g}/\text{dNm}^3$ at 3% O_2	18.0	15.3
	Oxidized Hg	% of Hg^{T}	11	1
FGD Inlet	Total Hg	$\mu\text{g}/\text{dNm}^3$ at 3% O_2	16.0	13.7
	Elemental Hg	$\mu\text{g}/\text{dNm}^3$ at 3% O_2	11.6	8.0
	Oxidized Hg	% of Hg^{T}	27	42
FGD Outlet	Total Hg	$\mu\text{g}/\text{dNm}^3$ at 3% O_2	13.1	9.5
	Elemental Hg	$\mu\text{g}/\text{dNm}^3$ at 3% O_2	12.3	8.9
	Oxidized Hg	%	7	6
FGD Bypass	Total Hg	$\mu\text{g}/\text{dNm}^3$ at 3% O_2	14.82	14.40
	Elemental Hg	$\mu\text{g}/\text{dNm}^3$ at 3% O_2	11.57	9.70
	Oxidized Hg	% of Hg^{T}	22	33
Stack	Total Hg	$\mu\text{g}/\text{dNm}^3$ at 3% O_2		8.7
	Elemental Hg	$\mu\text{g}/\text{dNm}^3$ at 3% O_2		8.3
	Oxidized Hg	% of Hg^{T}		5

Hg^T reduction = 43%

Native Mercury Removal	Wet Coal Baseline Average	Dried Coal Average
	%	%
Native Hg ^T Removal Across APH/ESP	16	10
Native Hg ^T Removal Across FGD	15	35
Native Hg ^T Removal Across APH/ESP/FGD	31	38
Native Hg ²⁺ Removal Across FGD	74	86
Hg ²⁺ Re-emitted as Hg ⁰	33	17

Energy Flows: Coal Creek Station 2006



Gross Unit Heat Rate = 9,825 BTU/kWh
Boiler Efficiency = 80.8 %

Sensible Heat Loss = 7.7 %

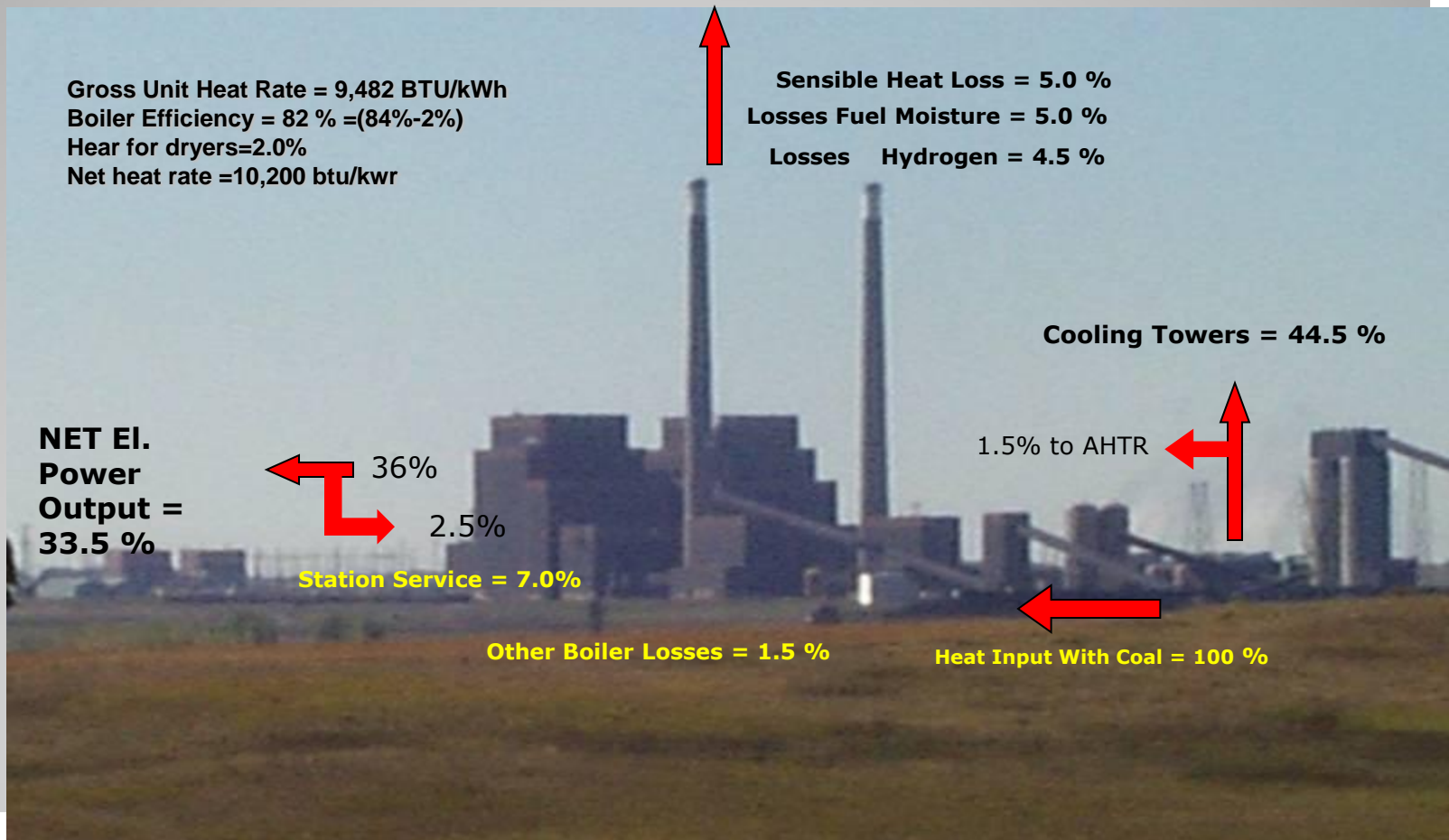
Gross Electric Power
Output = 34.73 %

Cooling Towers = 46 %

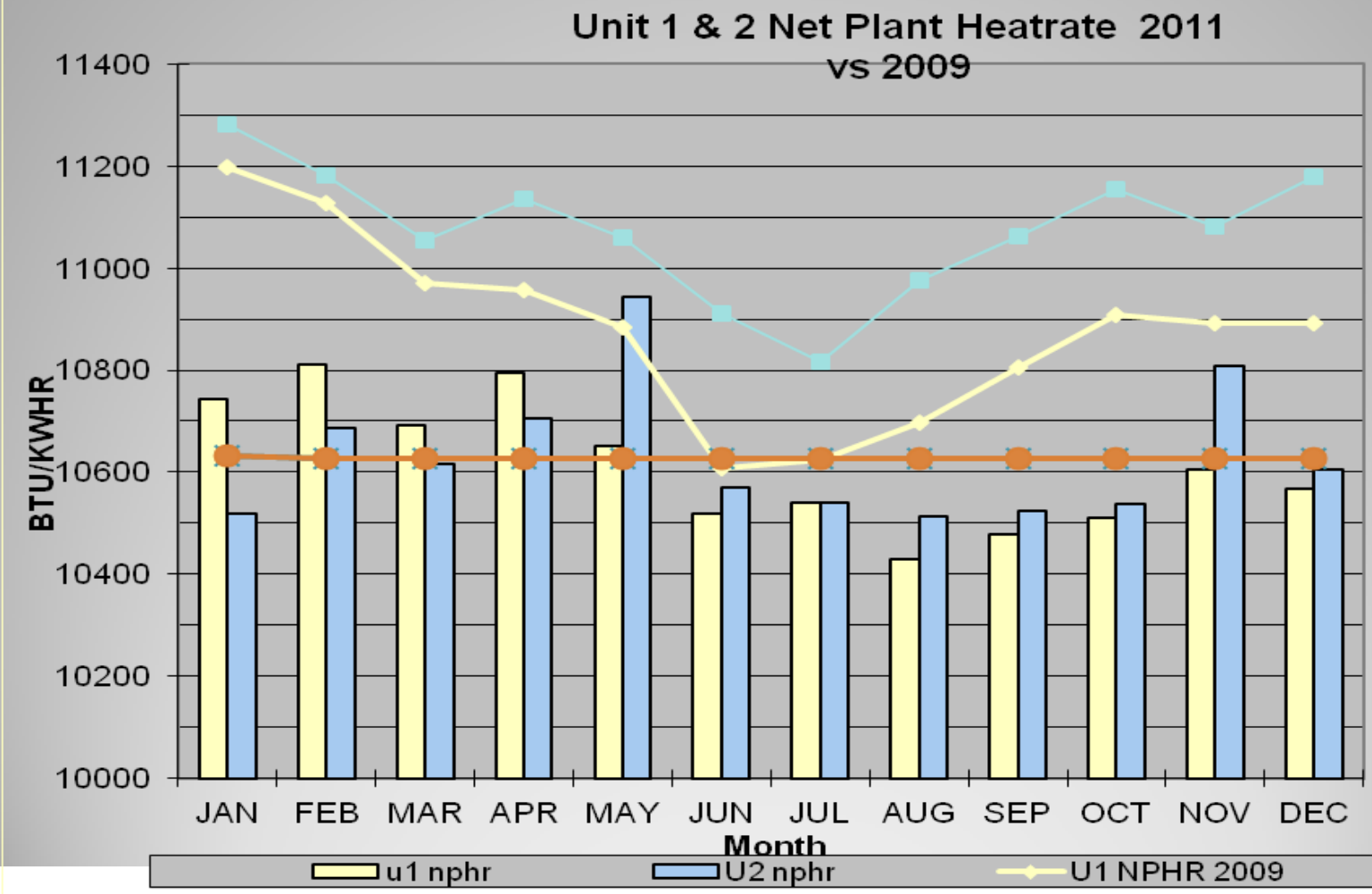
Evaporation of Fuel Moisture = 6.6 %
Hydrogen Losses = 4 %
Other Boiler Losses = 0.9 %
Station Service = 7.5%

Heat Input With Coal = 100 %

Heat Flows: Coal Creek Station 2013



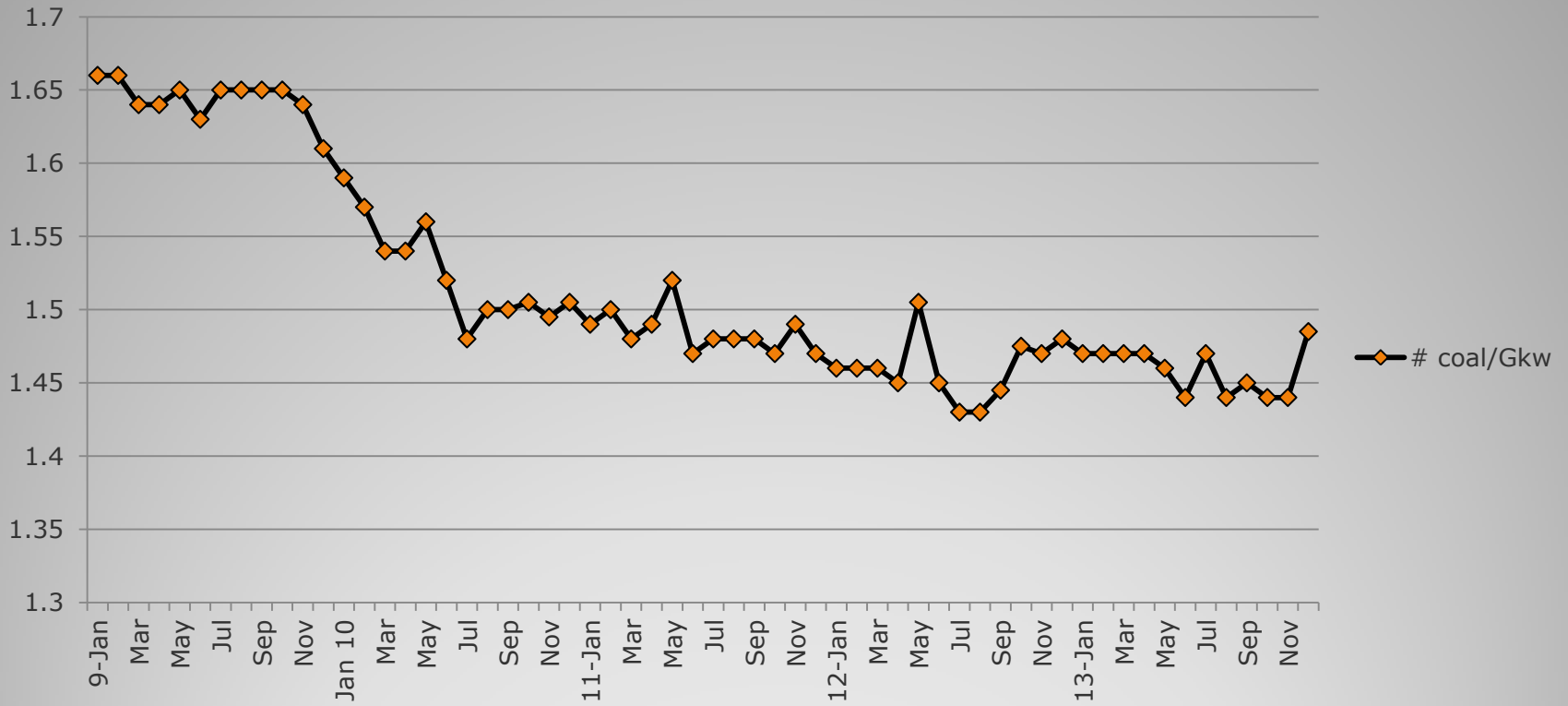
Seasonal heat rate improvement



DryFining results at Coal Creek

- ❑ **\$20+ million in annual O&M savings**
- ❑ **10% less fuel** – reduces O&M on fuel handling
- ❑ **54% less SO₂** - Segregation of ash minerals, plus improved collection efficiency, less coal flow
- ❑ **40% less Hg**- Segregation of ash minerals, plus improved collection efficiency, less coal flow
- ❑ **32% less NO_x**- Reduced volumetric release rate, improved air & fuel distribution to furnace
- ❑ **4% less CO₂**- 4% improved cycle efficiency
- ❑ Did qualify for a Section 45 coal production tax credit

coal/Gkw



Less coal per MW

2010 Coal-fired Project of the Year

